LECTURE NOTE

ON

REFRIGERETION AND AIR CONDITIONING(TH-5)

5TH SEM. MECHANICAL (DIPLOMA COURSE)



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of Agric Refriggerration cycle CHAPTER 1 It is defined as the process of Refrageriation :removing & maintaining a temperature well bellow that of surricounding * IN other worlds refrageriation 95 the process of cooling substance. UNAT OF REFRAGERICATION:-UNAT :- Tonne A tonne OF refrageriation as defined as amount of metragercation effect produced by the unaform metting of one tonne (1000 kg) OF 9CE From at 0°C 9D 24 hours. 1 TR = 1000 X 335 WZ 90 24 hours 1000 × 35 = 232.6 45/min = 24 X60 1 TR = 210 45/m 3.5 yw ore 3.5 47/sec 017 中心,后心,后心, The Seatthe 中国局部部制度制度

Definition of C.O.P :-

The co-effection of perchance (c. D.P) is the matrix of heat extracted in the refrigentation of the work done on the refrigement.

* It is also known as theoright cal co-efficient of peruportmance.

Theoretacal C.O.P = a

where, q = Amount of head-extracted

an the refragerators.

W = Amount of work done

* Perc writ may C. o.p =

* C.O.P 95 the neceptoral of the effectionary (1) of a heat engene.

Relative Co-efficient of performance The reation of the actual C.O.P to the theoretical C.O.P. 95 known as relative Co-efficient of performance.

Mathemats comy,

Relative C.O.P =

problem Find the c.o.p of a refragereation system of the work input, as southing and refragerration effect produce 95 160 42/49 of refragerant flowing. SOU" GTIVER W = 80 47/49 2/ = 160 4J/ 49 6 = 2 av C:0. p OF refrageration Refrigerating effect (R.E) ReFrigeriating effect is the heat absorbed In the evaporiatori per IbOF refragerant * If as determaned by the dafference an enthalpy of a 16 or refresgerant vapour leaving the evaporator and that OF a Ib of legined sust upstream (ahead) of the expansion value at the evaporatori * Refrigercation effect means that cooling action should be done at the rate of heat absorption from any place in a cyce.

Frankaple of working of open and closed System of refrigerration. APR cycle refrigerrations is one of the eardist method used For cooling the key Features of this method is that, the refrigerant arr remain gaseous state through out the representation cycle. Based on the operiation, the arra refragencies system can be clausefred anto. 1. open aare refrageration cycle 2. closed aare repragenation cycle. ore dense our reprogenation cycle open our reprogerention cycle ;--> In an open aure refrageration system, the arr 95 derectly passed over the space is to be cooled and allowed to canculate through the cooler. => The pressure of open refrugercation cycle 9\$ limited to the atmospheric. pressure.

rufriggeriation system :-=> In closed or dense air rufriggeriation cycle air rufriggeriant is contained within pipes and components part of the system of all the time.

that its large size !!!! > The agric supplied to the reprogenation system 95 large of Thus the size of the compressor and expanderc auso would be large. Another dazadrontages of the open cycle system as that the morsture is negularily caritad away by the canculating aarc, this leads to be the Formatgon of Frust at the end of the expansion preaced and cloge the line and hence a me of dyen is preferable to the open our refrageration system. * closed asra refragencition system/ Dense arra refrageration system :-

of once. D?s.advantages > one of the disadvantages of this system is

> If elemenates the need of a heat exchanger >> It is used in arritraft because it helps to pressure zation and arr. conditioning pressure zation and arr. conditioning

Advantages & applications

The cancellated airs does not have to observed contact with the space to be cooled, so the disodvombages instead in open airs refragencies can be elemenated.

-Advantages :-

> The suction to the compressor mary be of higher pressure therefore the volume of air handled by the compressor and expanden is smaller as compared to the open air system.

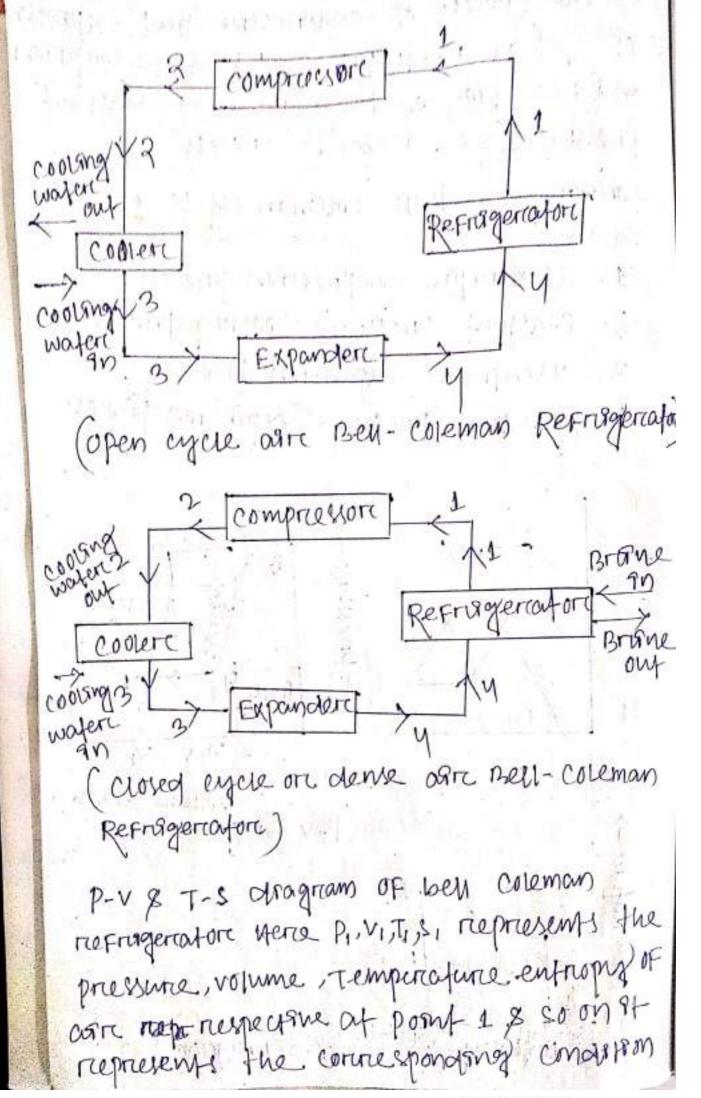
>> The chance of Freezeng of monster and choke the value of elemenated. >> In those system, higher co-effection of performance can be achieved by reducing operations pressure reafer.

Bell coleman cycle ?

Trevensed Brayton cycle on the Jone

The Bell- coleman cycle 9 & a refrigeration cycle where the worming Flund 75 arre which is compressed and expanded by but do not change stage state in this

The process of compression and expansion of gous is reentroppic and heat absorption and rejection of takes place at constant pressure (1. e. 7sobaria c process) working of Bell-coleman cycle: I senfropac compression process 2. constant pressure cooling process 3. Isentropac expansion process: 4. constant pressurce expansion priocess P2=P2 Isen. :33 R=Py V3 Vy V2 Mallar Make +volume (P-V Dragman) T2 Wart to I T33 4000 MBV - 1 si=s2)



of arre when it passes through the components I sentropic compression. process (1-2) The cold arrow from the representation 95 briought anto the compressor and comprises ed esentropecally during this process the pressure increment Friom PitoP2: The specarac volume decreases from vitov2 and the tempercature increments Friom I, to T2. during this process Entropy's stays steady (SI=S2). No heat 75 absorbed on rejected by OBTL. process (2-3) constant pressure cooling m process The worrow agre Frion the compressor IS then passed into the cooler where it is cooled at constant priessure, reducing. the temperature prion T3 to T2. The specific volume reduces From V2 to V2. Heat rejected by the asrc Qre = Cp (T2-T3) A Stat way to wat of the wat he was to be the (11) 1 公平射: 各

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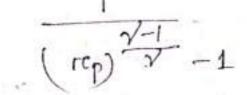
= Heat respected - year absorbed Cp (T2-T3) - Cp (T1-T4)

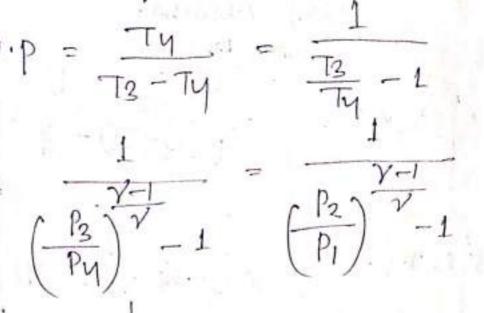
place in this process. priocess(y-1) constant pressure Expansion -> Durang this process pressure of arre is constant and temperature increases From Ty to TI and specific volume ancrieases prion vy to vi -> weat addression by arre takes place In this process during constant priesson perc Mg OF. 0972. Qy-1 = Cp (T1-Ty) (CP) orn = 1.005 43/49-4] worundone during the cycle percing of win

process (3-4) Isenfropac expansion APTE FROM the Cooler 95 presenting brought anto the expander and "as extended Fsentroppicany the pressure of arr stays decreases From P3 to Py . specific volume increases from v3 to vy and tempercature décréaises prion T3 to Ty. 7 No hear addrison on nesection fames

C. O. P during the cycle per up of arr Heat absorbed woringone cp (T1 - T4) . 0: P Cp (T2-73) - Cp (T1-T4) (T1 - TY) C. O. P. (T2-T3) - (T1-T4) Ty (-1). C. 0. P = T3 (73-1) - Ty (-1) Force gentropac comprission process(1-2) $\frac{T_2}{T_1} = \left(\frac{P_2}{P_1}\right)$ Forc resentruper expansion process (3-4) $\frac{T_3}{T_4} = \left(\frac{P_3}{P_4}\right)^{-1} - \frac{T_3}{T_4} = \left(\frac{P_3}{P_4}\right)^{-1} - \frac{T_4}{T_4} = \left(\frac{P_3}{P_4}\right)^{-1} - \frac{T_4}{T_$, FROM. since, P2 = P3 & P1 = Py there force ean (1) and (1) $T_2 = \frac{T_3}{T_3} \quad \text{orc} \quad \frac{T_2}{T_3} = \frac{T_4}{T_4}$ KTH AND THE HAVE AND - Air

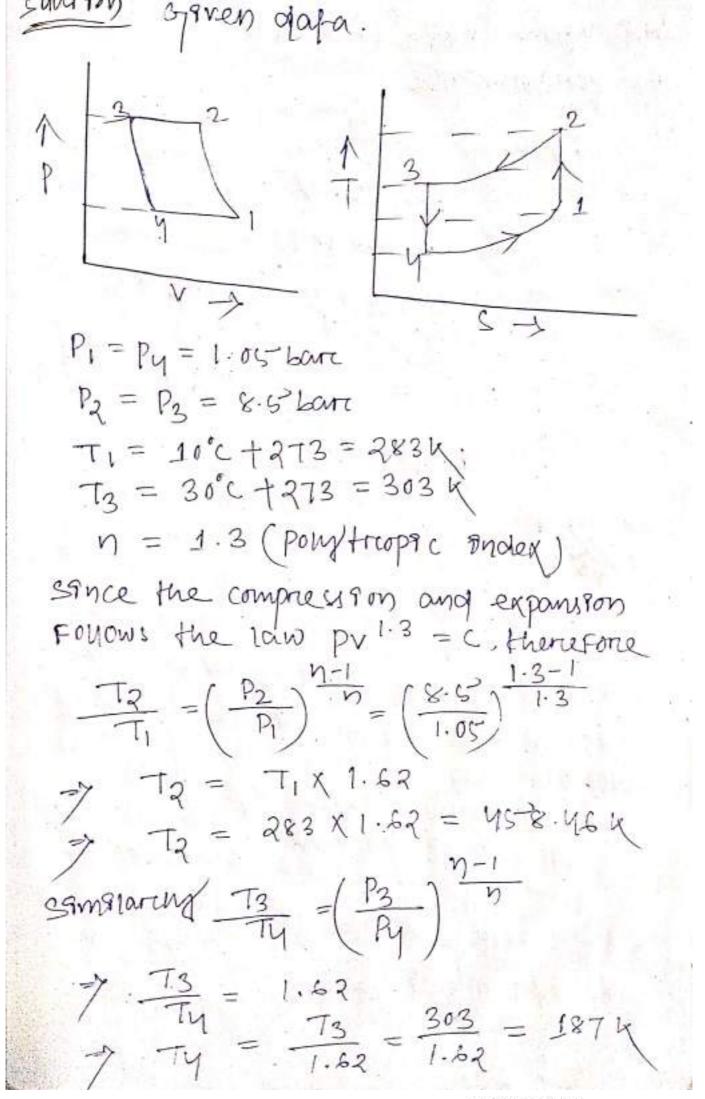
comprisession ore Expansion = 12 = = 120490 prublem -In a refrageration plant worowing on Bell-coloman cycle, arr 95 compressed to 5 bari From 1 bari. Its 9ng Had temperature 95, 10°C. After compression, the arra of cooled up to 20°C on a cooler before expanding ball to a pressure of 1 barc. Defermine the theoretical cop of the plant and net reprogerating effect. Tank cp = 1.005 hJ/kg h and cv = 0.7184





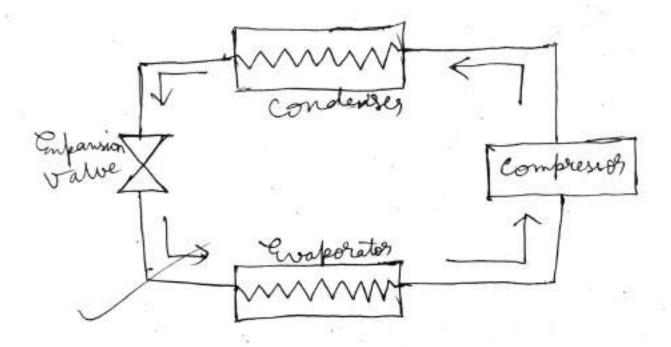
gaven data. control P2 = P3 = 5 barc P1 = Py = 1 barc T, = 10°C + 273 = 2834 T3 = 20°C + 273 = 293 K cp = 1.005 45/194 cv = 0.718 47/49/4we know Isenfrip 9 c . Index 1.005 = 1.9 V = CP = 0.718 Force gentrupgic compression process (1-2) 1.4-1 V-1 1) 1.4 T2 = (P21) 7 = (5 The Aller 0.286 1.584 -(5) = T, X 1.584 = 283 X 1.584 T2 = 448.272 KP

For asentropac expansion process $\frac{T_3}{T_4} = \left(\frac{P_3}{P_4}\right)^{\gamma} \frac{\gamma}{\gamma}$ 1.4-1 293 1.4 (5)1850 1.584 Ty we ynow that C. O. p OF the plant = T2-14 185 1.713 293 - 185 Net-refragerant effect R.E. = Cp (t1 - Ty) = 1.005 (283-185) 98.5- 42/49 Ans. 3. A refrigeratori working on Bell-Coleman aycie operates bet pressure 19mats of 1.05 bare and 8.5° bare. APT 95 grawn From the cold chambers at 10°C, compressed and then It is cooled to so c before entering the expansion ciginder. The expansion and compression Follows the law pv 1.3 = constant Defermine the theorders car C. o.p. of the system



co-efficien we know that theorieff cal OF perc Formance C. O. V-1 283 87 -1) (458.02-303) 1.3 (1.3 187) 2 (Taying V = 1. 1.28

Simple Vapour Compression Reprigeration Cycl Mechanism of a simple Vapour Compression reprigeration System (VCRS)

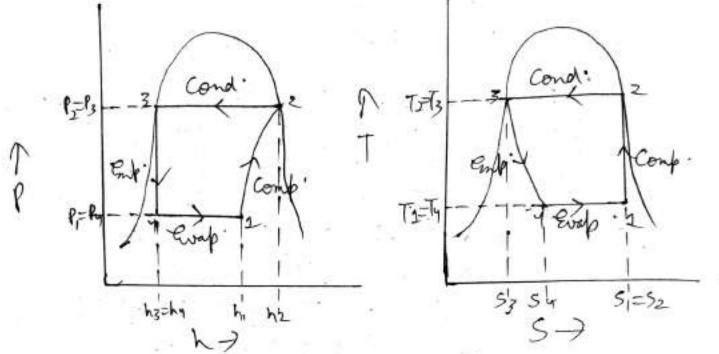


Compressor: -The low pressure and temperature vapour refeigerant from evaporator goes to compressor through inlet value then in compressor low pressure and temperative compressed to a high pressure and temperature vapour referigerant is discharged into the condenses through delivery value.

Condenser : the high pressure and temperature vapour reprigerant change into fluid medium. The refrigerant gives it's latent heat to the sevroun. ding condensing medium which is normally air or water Enpansion value:-It is also called reprigerant control value. The punction of the enpansion value is to Anpand the reprigerant from high pressure of temperature to low temperature. Evapolator :-An evaporator consists of coils of pipe in which the liquid vapour reprigerant is evaporated and changed into vapour reprigorant at low pressione and temperature. In evaporating the liquid vapour reprigerant absorbs it's latent heat of vapourisation which the medium (ais, water or beine) is to be cooled.

1) Mention the advantages of Vapow, Compression Repriferation System over Air Compression Repeigeration System. Describe the mechanism of a a) Simple on Vapour compression Reprigeration System: (i) Cycle with dry satisfied vapour after compression (i) Cycle with wet vapour after (ii) Cycle with wet vapour after compression. compression. (iii) Cycle with superheated vapour after compression. (iv) Cycle with superheated vapour before compression. (i) Cycle with under-cooling or sub-cooling of reprigerant.

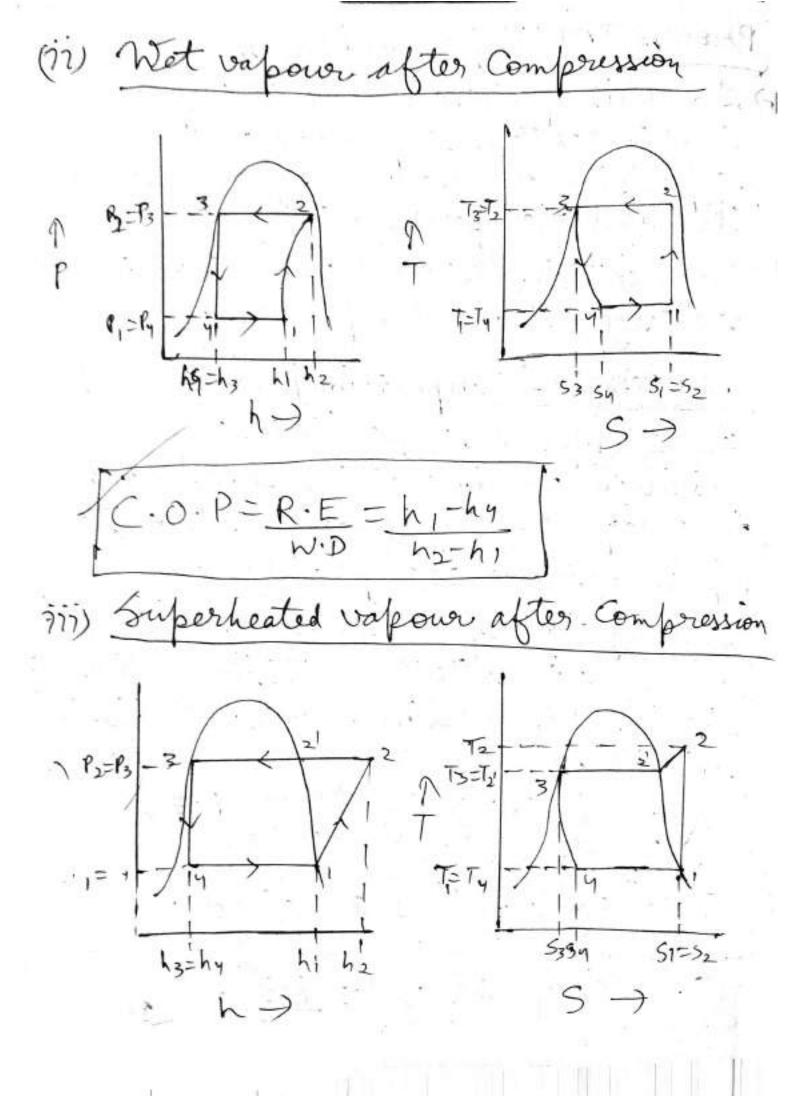
Types of Vapour Compression Cycle (VCR) i) Dry Saturated Vapour after Compression



(Process 1-2) Compression Process > The vapour reprigerant at low pressure (P1) and temperature (T1) is compressed isentropically to dry saturated vapour. =) Workdone happens during this process and is done on the system. > Workdone = h2-h2

(Process 2-3) Condensing Process In this process the high pressure and temperature vapour refrigerant is Condensed at Pressure P2.

(Process 3-4) Enpansion Process In this process the liquid vapour reprigerant is enhanded through enhansion valve to a low pressure (P3) and temperature (T4). =) No heat is absorbed or rejected by the refergerant in the process. (Process 4-1) Evaporation Process I In this process the liquid vapour, minture reprigerant is evaporated to vapour reprigerant at constant pressure and temperature. =) During this process the refrigerant absorbs its latent heat of vaporisation from the medium (ais, water, brine) which is to be cooled. =) So refrigerating Effect (R.E) =hg-hy =) The cycle is this repeated C. O.P of the cycle= R.E = 41-47 W.D hz-hz



h,-hy W·D hj-hj (iv) Superheated vapour before comp resson Te T3 Pz=1, Picty h1 12 hz=hy Sz 51=52 P= R·E = h, - hy h2-h1 W.D apour Compression with Sub- Cooling (v)てもしち 2 B=B 1, 12 51=52 hzshy 5354 $D \cdot P = R \cdot E$ h, W.D h2-h

Advantages of Vapour Compression reprigeration Gystem over Ais Compression reprigeration system :-1) It has smaller size for the given capacity of reprigeration: 2) It has less running cost 3) It can be employed overa large range of temperatures. 4) The coefficient of performance is quite high Firadvantages 2) The initial cost is high 2) The prevention of leakage of the reprigerant is the major problem in vapour compression system.

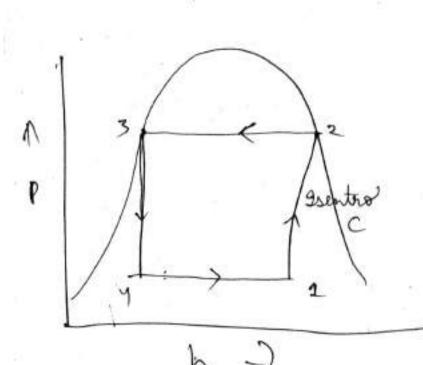
In an ammonia vapour compression the pressure in the evaporator is 2 bag. Ammonia at lant is 0.815 day and out the entry its dryners praction is 0.19. During compression the work done per kg of ammonia is 150KJ. Calculate the C.O.P and the volume of vapour entering the compresso per minute . If the state of ammonia conculation 4.5 kg por min. The latent heat and specific volume at 2 bar is 1325 KJ/kg and 0.5 8 m3/kg Ans: - Criven data: -P1=Py=2 0007 $m_1 = 0.85$ $m_1 = 0.19$. $W \cdot D = 15 O K J$ Rate of ammonia conculation = 4:5 kg/mi

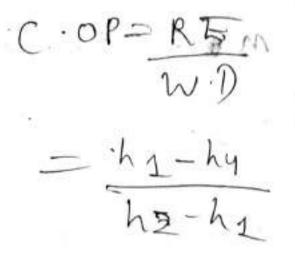
"HDL. H = 1325 K5/kg (Vg) Specific volume = 0.5 8 m3/kg Prefe Pr 5-) 51=52). h_= hf + (mxh. fg). $= 117.69 + (0.85 \times 1325)$ = 1293.941<5/kg thy=hft(myxhfg) = 117.69+ (0.19×1325) = 369.44 K5/kg RE=h1-hq= 8.79.5 kJ/kg C.O.P=RE = 874.5 = 5.83 WD compressor per min = Mass of Refrigerant per min XS. IV = 4.5 kg/min × 0.58 gm3/kg = 2.61 m/min

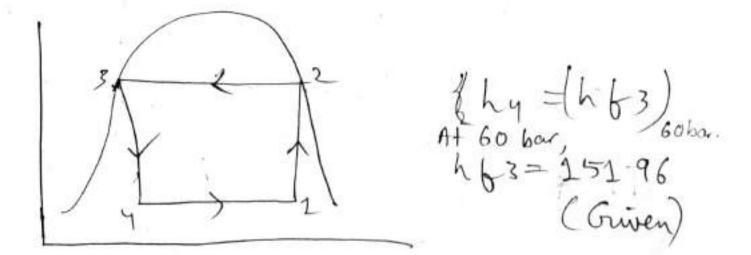
A vapour compression refigerato 60 bas and 25 bar. The working fluid is just day at the end of compression. There is no undercoding of liquid before enpansion value. Letermine (i) C.O.P if the blind flow is at a rate of 5 kg/min: Ans:- Given data: " Pressure Sat temp Enthalpy Enteropy (var) (K) Liquid Vapous Liquid Vapous 60 295 191.96 293.23 6.554 1.032 25 267 86.32 32258 0.25 2.264 $\frac{1}{OP} = R \cdot E = h_1 - h_1$ WD A 2-41 hi= hftmintg) soag

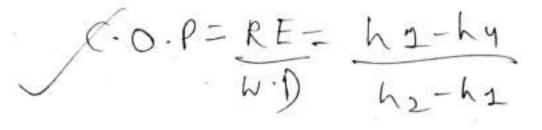
M = 51=52 =) 1.0332 = 0.226 + mx 1.0204 -) m= 0.791 hy=hft(mxhfg) at 25 bas hfg = 322.58-56:32 266.26 56.32 + (0.791×266.26) him = 266.93 KJ/kg









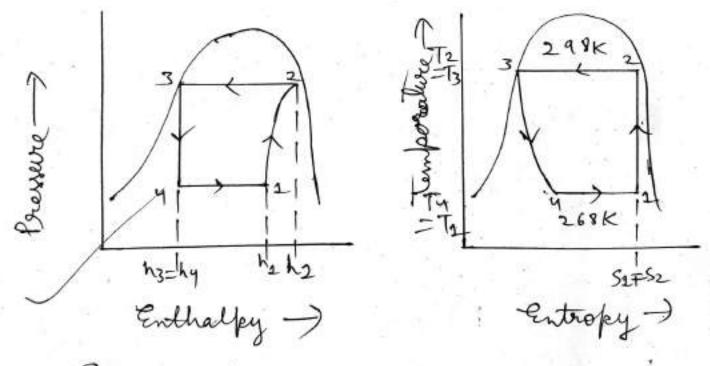


266.93-151.96 2 93.23 - 266.93 4.36

(i) apacity of refrigerator -Referigerating effectet =h1-hy = 266.93-151.96 = 114.97 KJ/kg Rate of flow = 5 kg/min) 114.97 X5 = 574.85 KJ/kg 1TR = 210 KJ/min) (apacity = 574.85 = 2.73TR

Find the theoretical C. O. P for a Co2 machine working between the temperature range of 25°C and -5°C. The dryners praction of CO2 gas during the suction stroke is 0.6. Following properties are given for CO2

Temp .	Liquid		Vapouri		Latent
•	Enthalfy KJ/kg	Entropy KJ/KJ-K	Enthelpy (kJ/kg	Entropy KJ/kg-K Lsgy	heat kJ/kg (hbg)
25	264.77		2.82.23	0.9918	117.46
-5	72.57	0.2862	32233	1.2146	248.76



Griven data $\exists T_2 = T_3 = 25^\circ c = 25 + 27^3 = 298K$ $\exists T_2 = T_3 = 75^\circ c = -5 + 273 = 268K$ $\exists T_3 = T_4 = -5^\circ c = -5 + 273 = 268K$ $\exists M_1 = 0.6$

 $C \cdot O \cdot P = R \cdot E$ WD =) h1-h4 h2-h1

h1=hfitm1*hfg1 = 72.57+0.6×248.76 = 221.83 K 5/kg $hy = hf_3$ = 164.77 KJ/kg h2= Mf2+m2 Xhfg2 To find n2 (dryness graction at point 2) S1=S2 S1= 5/52+ MX + 69/2 = 0.2862+ 0.6× (~g-~b) = 0.2862+ 0.6× (1.2146-0.2862) = 0.843 Since S2=S2 therefore:-52= 0.843 -) S2 = Sf2+ M2× 8692 =)0.843 = 0.5978 + M2× (0.9918 -0.5973)

=) M1= 0.622 45 ¹⁴ L Now $h_2 = h_b_2 + m_x (h_b_g_2)$ = 164.77+0.622X (117.46) = 237.83 KJ/kg $(\cdot \circ \cdot P = h_1 - h_9)$ h > - h 1 221-83-164.77 237.83-221.83 3.56 (Aus)

Q2) A vapour compression reprigerator liquid evaporates in the evaporatos at 15°C. The temperature of this reprigerant at the delivery from the compressor is 15°C when the tapour is condensed at 10°C. Find i) there is no undercooling, and (i) the liquid is cooled by 5°C before enpansion by throttling

Temperature	Enthalpy in KJ/kg		Specific entropy in KJ/kg	
m°C	Liquid		Liquid	Vapous,
-15	22.3	1.80.88		0.7051
10	45.4	291-76	0.1750	0.6921

chy: - Oriven data.

 $T_1 = T_4 = -15^{\circ}C = 258 K$ $T_2 = T_3 = 10^{\circ}C = 2.83 \text{ K}$ 12=15°C = 288K Cpv= 0.64 KJ/kg K CP1=0.94 K J/kg K (1) Let m= dryness praction at point Entropy at point 2 = S1 S1= sf1 +mx sfg1 = sf1+ mix \$(sg1-sf2). = 000000 0.904 M20.6147 Entropy Xat point 2 7 52

82=× (+ m, X (× + ~ (/2)

= (0.1750)+m, × (0.6421

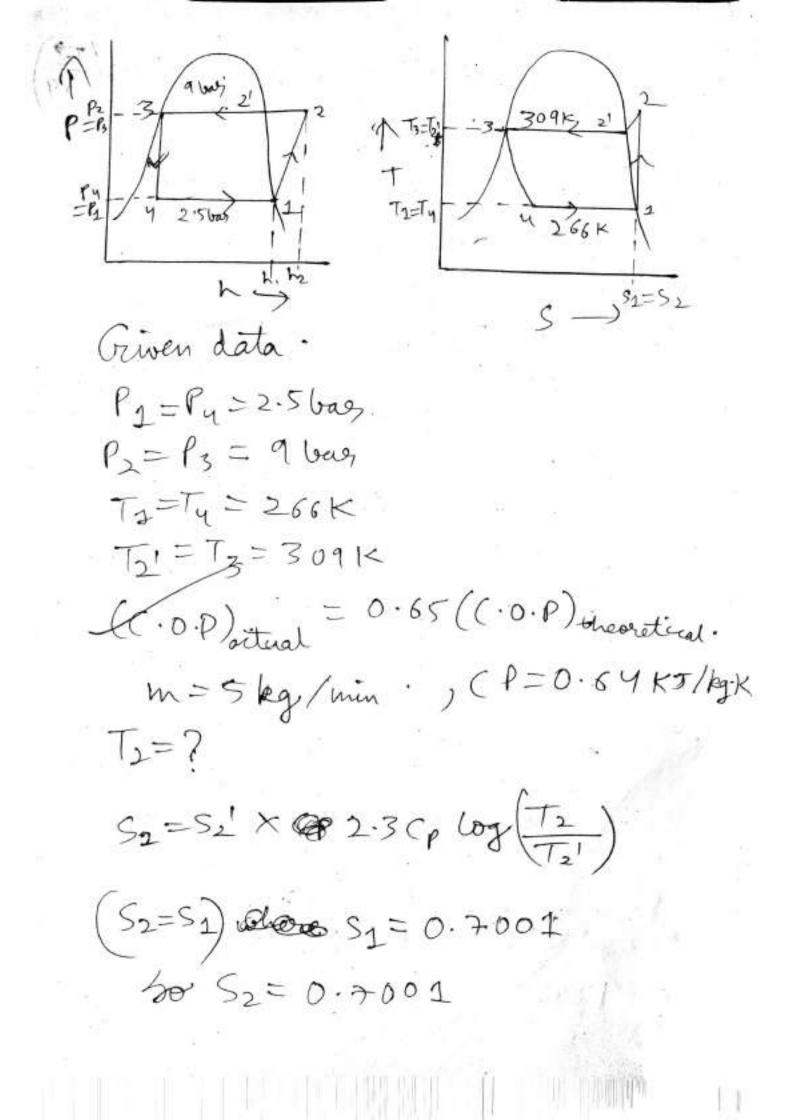
Entropy at point 2=S2 $S_2 = S_2' + 2.3 C_{p_1} \log \left(\frac{T_2}{T_2} \right)$ 0.6921+2.3×0.69 log (285) $(: S_2' = sg_s)$ 7032 We know that S1 = S2 \$ 0. yx x Mg - 0.7032 $0.0904+m_10.6147=0.7032$ JM1= 0.996 ni hathy

Now. h_= hf2+mxhfg2 = AC 22.3+ 0.996× (180.88-22.3) = 180.24 KJ/kg $h_{1} = h_{2}' + CP_{v}(T_{2} - T_{1}')$ - 191.76+0.64(288-283) (... h_1' = hg hg -) = 1 94.96 KJ/kg My= 1 +3 = 45.4 C. OP = RE h1-hy $h_{2} - h_{1}$ W.D 180.29-45.4 194.96-180.24 = 9.16

(ii) Coefficient of performance when there is an undercooling of 5°C 3 hy=hf3 (degree of cooling hb3=hb3'-CP1×5 45.4-94X5 40.7 $(.0.P = RE = h_1 - h_1)$ D h2-h2 W 180.24-40.7 94-96-180.24 = 9.47

32) A reprigeration machine using R-12 as reprigerant operates between the pressures 2.5 and 9 bar. The compression is isentotopic and there is no undercooling in the condenser. The vapous is in day saturated condition at the beginning of the compression. Estimate the theoretical coefficient of performance If the actual coefficient of performan is 0.65 of theoretical value, calculate the net cooling produced per Now. The refeigerant flow is 5 kg per minute. Peroperties of refrigorant are:-

Pressure	Sat temp,°C	Enthalpy, KJ/By		Entropy of sat unlang
		Liquid	Vapow,	Entropy of sativation
9-0	36	70.55	201.8	0.6836
2.5	-7	29.62	1.84.5	0.7002
	×			A CONTRACTOR OF THE



D0.7-001=0.6836+2.3×0.646 -> log(T2) = @@eta 0 7001-0.6836 2.3×0.64 =) log (=== 0.0112 $=)\left(\frac{\tau_{2}}{\tau_{2}}\right) = 10^{0.0112} (\log^{-1})$

= $\left(\frac{T_2}{309}\right) = 1.026$ -) T2= 1.026×309=317K

 $h_2 = h_1' + c_p(T_2 - T_2')$ = 201.8+ 0.64 (317-30g) $f(h_2) = hq_2$

= 206.92 KJ/kg

(C.OP) theoretical = him hand

= 184.5 - 70.55 (. hy=h63) 208.92 - 184.5

 $(C.0.P)_{th} = 5.08$ (. 0. P) actual = 0.65× (5.08) =3.30 $WD = h_2 - h_1 = 206.92 - 184.5$ = 22.42 KJ/kg Net Cooling (R.E) = COPXW.D = 3.30×22.42 =73.98×5/kg R.E per hour = 73.98×5 = 369.9 (1TR = 310 KJ/min) $=) \frac{36999}{210} = 1.76$ R.E per hour = 1.76 TR

Chapter-3 Vapour absorption Refrigeration System (VARS) =) The vapour absorption reprigeration system is one of the oldest method, of producing reprigerating effet. =) It may be used in both the "domestic and large industrial reprigerating plants. =) It uses heat energy instead of mechanical energy as in vapour compression systems, in order to change the conditions of the reprigerant required for the operation ajde. =) In VARS, the compressor is replaced by an absorber, a pump, agéneratos and a pressure reducing value. =) The refrigerant commonly used in VARS is ammonia.

91) With neat sketch describe simple Absorption System Cooling y rejected (Q) Ans:-Condenser F + Biquid Generator Supplied (QG) Receiver O Pressure preducing value Empension 7 7 >0 Punt Auserber & Ewaporator & & Cooling V water yeat rejected (QA) (Simple Vapour Absorption System) () The simple vapour absorption system, consists of an absorber, a fromp, a generator and a pressure reducing value to replace the compressor of vapour compression system (ii) The other components of the system are condenser, deceiver, enpansion

Value and evaporator as in the Vapour compression system. (771) In this system, the low pressure ammonia vapour leaving the evaporator enters the absorber where it is absorbed by the cold water in the absorber (1V) The water has the ability to absorb very large quantities -of annonia vapour and the Solution, thus formed is known as aqua- aminoria. (V) The absorption of ammonia vapous, in water towers the pressure in the absorber which in turn draws more ammonia vapour from the evaporator and thus raises the temperature of solution. (VI) the strong solution thus formed in the absorber is pumped to the generator by the liquid pump (vii) The strong solution of ammonia in the generator is heated by

some enternal source such as gas or steam "(Viii) During the heating process, the ammonia vapour is driven off the solution at high pressure leaving behind the hot weak ammonia solution in the generator. (1X) The weak ammomia solution flows back to the absorberat low pressure after passing Abrough the preisure reducing Value (x) The high pressure ammonia vapour from the generator is condensed in the condenses to a brigh pressure liquid amnonia. (x) This liquid ammonia is passed to the enpansion value through the receiver and then to the evaporator. (xii) This completes the simple Vapour absorption cycle.

B2) Advantages of Vapour Absorption Reprigeration System over Vapour i Compression Referigeration System. Ans:- i) In the vapour absorption system the only moving part of the entire system is a pump, thus its comparatively quieter and is subjected to little wear. (11) The VARS uses heat energy whereas VCRS uses mechanical energy (11) Electricity is a necesity in VCRS

but in VARS no electricity is required as it operates on waste heat.

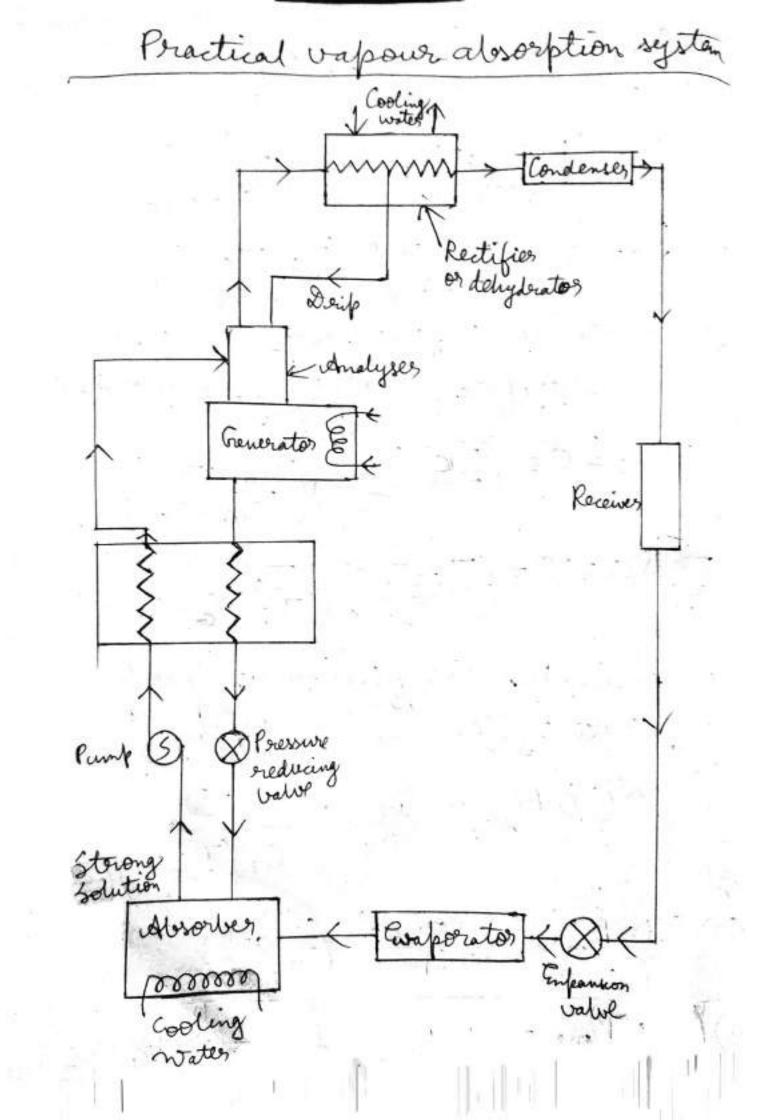
(iv) Ioad Variations do not affect the performance of a vapous absorption system whereas. performance is preduced in VCRS when partial loads are poos. (v) In VARS the liquid referigerant leaving the evaporator has no bad effect on the system but in

VCRS it is necessary to superheat the vapour reprigerant leaving the evaporator so that no liquid may enter the compressor. (VI) The vapour absorption systems can be built in capacities well above 1000 tonnes of refrigeration each, which is the largest size for single compressor units (VI) The space requirements and automatic control requirements favour the absorption system more and more as the desired evaporatos temperature drops. Control Parts X1 (2) 718 . - 20 The mark

Simple Vapour Absorption System HPAV 6 Crenerator Heat Sulpplied (Qon) Condenses (liquid Steam Wheat Sulpplied (Qon) Condenses (liquid Steam Wheat Heat He Cremeratory Aleak Solution Steam 4 Meak Solution heating will Prevouve nequilating Value 4 Heat 2 Alexender 2 LPAV Evalporator 8 Solution Cooling Heat rejected (QA) Coefficient of Performance of an Ideal Vapour Absorption Reprigeration Surtem System a) QG = heat given to the refrigerant in the generator b) Qc = heat discharged to the from the condenser and absorber. C) Q = = heat absorbed by the refrigerant in the evaporator d) Qr= heat added to the refrigerent due to pumpwork.

Neglecting the heat due to pumpwork! (QP) we have Qc=QGit QE (According to the first law of the modyneming Set TG= Temperature at which heat is given to the generator Tc = temperature at which heat is discharged to atmosphere E = Temperature at which heat is absorbed in the evaporator. In a perfectly reversible system, the initial entropy of the system must be Aqual to the entropy of the system after the change in its condition. Since VARS is considered as a perfectly $\frac{Q_G}{T_G} + \frac{Q_E}{T_E} = \frac{Q_C}{T_C}$ $= Q_{G} + Q_E (Q_C = Q_G + Q_E)$ $=) \frac{Q_G}{T_G} + \frac{Q_E}{T_E} = \frac{Q_G}{T_C} + \frac{Q_E}{T_C}$

 $=) \frac{Q_G}{T_G} - \frac{Q_G}{T_C} = \frac{Q_E}{T_C} - \frac{Q_E}{T_E}$ =) $Q_G\left(\frac{T_C-T_G}{T_G \times T_C}\right) = Q_E\left(\frac{T_E-T_C}{T_C \times T_E}\right)$ $\Rightarrow Q_G = Q_E \left(\frac{T_E - T_c}{T_c \times T_E} \right) \left(\frac{T_G \times T_c}{T_c - T_G} \right)$ Since TG>TC>TE
Cherefore multiplying we we get. $=) Q_{G} = Q_{E} \left(\frac{T_{E} - T_{E}}{T_{C} \times T_{E}} \right) \left(\frac{T_{G} \times T_{C}}{T_{G} - T_{C}} \right)$ $\exists Q_G = Q_E \left(\frac{T_c - T_E}{T_E} \right) \left(\frac{T_G}{T_G} \right)^2$ Manimum coefficient of performance of the system is given by $(C \cdot 0 \cdot P)_{man} = \frac{Q_E}{Q_E} = \frac{Q_E}{Q$ =)(C.O.P)main = (TOTE) (TOTE) TCTE) (TOTO))(C.O.P)main = C.O.P (suefrigerato) X C.O.P (Heat Engine)



(i) The Simple ator vapour absorption system is not very economical. In order to make it practical, it is fitted with an Analyses, Rectifies and a Heat Enchanger . (1) When the low prossure ammonia. vapour leaving the wapprator enters the cold water present there thus forming a strong aqua-ammonia solution iii) This strong solution is then pumped to the generator by the pump provided. (iv) This strong solution of ammonia in the generator is heated by heating coils by which ammonia vapour is driven off leaving behind the hot weak solution which flows back to the absorber. (1) The heat enchanger provided between the absorber and the generator then cools the weak hot solution returning to the absorber. (vi) The heat removed from the weak solution raises the temperature of

the storing solution going to the generiator ishich in turn reduces the heat supplied to the generator and cooling required at the absorber making it more economical : (Vii) When Ammonia is vapoured in the generatory some water is also vaporised and will flow into the condenser which can piege and choke the pipeline. (VIII) In order to remove these thewardes water particles, an analyser is used which may be an integral part of generator or attached externally. (ix) In consists of a series of trays mounted above the generator to which the strong solution from the absorber introduced and flows downward over the trains into the generator. (x) In this way, considerable liquid surface area is enposed to the vapour rising from the genera - tor and most of the vapour

Condenses (XI) In case the water vapours are not completely removed in the analyses, a closed type vapour cooler called pietifier or deligdrator is used. (Xii) It's function is to cool further the ammonia vapours leaving the analyses so that the remaining water, vapours are condensed and only dry aminonia vapour flows to the condenses. XIII The condensate from the rectifies is returned to the top of the analyses, by a drip return pipe (XIV) Then the high pressure ammonia vapour is condensed in the condenses to a high pressure liquid ammonia. (xv) This tiquid ammonia is passed to the enfansion value through the receives and then to the evaporator which turns it into two pressure vapour ammonia (xvi) This cycle is thus repeated ,

(32) In a vapour absorption refriger. - ation system, heating, cooling and refrigeration take place at the temp. - vatures of 200°C, 20°C and -5° c respec -tively Fing the manimum C-0. Pof the system Ans: - Given data · TG= 100°C = 373K $T_c = 20^{\circ}C = 293 K$ TE= -5°C = 268K $(-OP_{(man)} = \left(\frac{T_E}{T_C - T_E}\right) \cdot \left(\frac{T_G - T_C}{T_G}\right)$ $= \left(\frac{268}{293 - 268}\right) \left(\frac{373 - 293}{.373}\right)$ =2-2.9

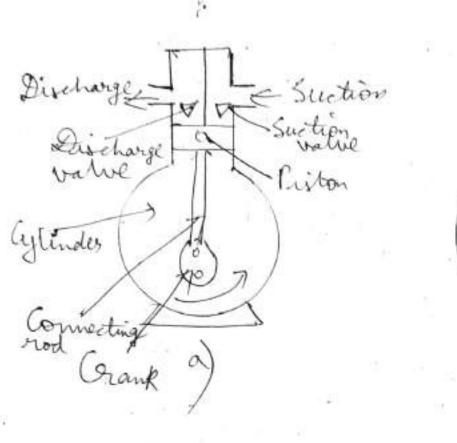
Chapter-4. Réprigérant compressor :-Function :-A reprigerant compressor is a machine which is used to compress the low pressure and low temperation and converted into high pressure and high temperature vapour refrigerant. Classification of Compressor: 1) According to method of compression a) Reciperocating compressor b) Rotary compressor () Centrifugal compressor. 2) According to no of working strokes! a) Single stage compressor. 6) Double acting compressor

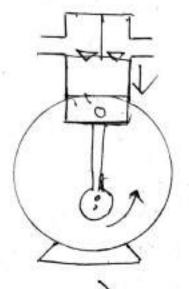
3) According to no of stages a) Gingle stage D'Multi stage ") According to the method of doive a) Direct drive compressors 6) Belt drive compressors 5) According to the location of the prime moves a) Semi-hermétic compressors b) Hermetric compressores. Important terms 1) Suction pressure :- It is the absolute pressure of reprigerant at the inlet of a compressor. 2) Dircharge pressure: It is the absolute pressure of refrigerant at the outlet of a compressor. 3) Compression ratio :- It is the ratio of absolute discharge fressione

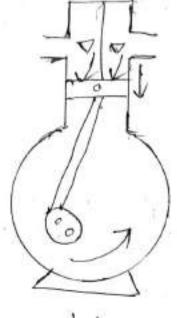
to the absolute suction pressure. Since the absolute discharge pressure is always more than the absolute suction pressure, therefore, the value of compression ratio is more than unity =) The compression ratio may also be defined as the ratio of total cylinder volume to the clearance volume. 4) Suction volume :- It is the volume - of during its suction stroke. It is usually denoted by 1/5. 5) Piston displacement volume or stroke volume or swept volume :-It is the volume swept by the piston when it moves from it's top or inner dead position to bottom or outer dead centre position. Vp= XDXL D = diameter of cylinder, and L= Length of piston strake.

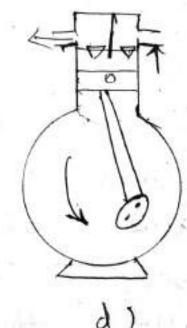
6) Cleanance factor :- It is the ratio of dearance volume (v.) to the piston displacement volume (Vp). Mathematically, cleanance factos. = Ve 7) Compressor capacity :- It is the volume of the actual amount of reprigerant passing through the compressor in unit time. It is equal to the suction volume (V.). It is tappressed in m3/s. 8) Volumetoice efficiency :- It is the ratio of the compressos capacity or the suction volume (Vs) to the piston displacement volume (1p). Mathematically, volumetri, efficiency. I A good compressor has a volumatric efficiency of 70 to 80 percent.

reciprocating Poinciple & Working of compressors









=) A reciperocating compressos consider of a piston and cylindes the piston is deriven through a connecting rod & orank. =) It consists of two values inlet and outlet. These values mounted on cylinder head and operating due to pressure difference -=) The working of reciprocating compressor complete in two stroke of piston or one revolution of crank shaft =) During suction storoke, the piston moves downward and inlet value open and outlet value closed due to pressure difference between cylindes and surrounding. Then the low pressure seek in the engine cylindes through inlet value. I Now, this stocke piston moves upward the slight increase in ajlinder pressure will cause intet valve closed and enhaust volve closed

=) Now piston reaches the top, the pressure inside the cylindos will be high as compared to discharged value. Then the discharge walve gas opened and the vapour refrigerant is discharged into the condenses, and this cycle is expected 2 Isentropie - Polytropic Isotheornal Poressure Valerme. (P-V) diagram Isentropic Polytropic goothermal Temperature Entropy ?? (T-S) diagram

Aermetically Sealed Compressor I when the compressor and motor operate on the same shaft and are enclosed in a common casing, they are known as hermetic sealed compressors =) The hermetic sealed compressors are widely used for small capacity reprigerating systems such as in domestic reprigerators, home preezers and window air conditioners Advantages: -1) The leakage of refrigerant is completely prevented. 2) It is less money 3) It requires small space betause of Compactness. 4) The Inderication is simple as the motor and compressor operate in a sealed space with the Inderi-- Cating oil

Disadvantages: -1) The maintenance is not easy because the moving parts are inaccessible. 2) A separate pump is required for evocuation and charging of refriger Rotary Compressors :-1) Single stationary blade type rotary compressor Housing Direberg 7 aylindes Eccentric Black - Roller (Impelles) met Sapour. referigerant Suction Rotor shaft

15 1 14

=) A stationary blade type rotary compressor consists of cylinder rolle, and a shaft and a spring loaded blade . =) The centre of the shaft coincides with the centre of the cylinder. =) Roller is in the closest possible contact with the wall of the cylindes and the point of contact sums around the cylinder as shaft and roller rotate. =) The inlet is separated from the which remains in contact with the roller. > Due to the eccentrically between roller and cylinder the clearance between them is not uniform. > The whole assembly is placed in an air tight casing and submerged in an oil both.) when the space permits low pressure repigerant wapour from the evaporator enters the cylinder.

) As the roller notates, this referi--gerant vapour is compressed until it's pressure forces open the discharge value and the high pressure vapour flows towards the condenses. 2) Rotating blade type rotary compressos to condenses Rotos Rotos Value Discharge - Rotor shaft (houge, Suction From Port evaporator

=) In this design the motor shaft is set off centre with the cylinder and, is arranged co= anially with a

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notos which is notating around the inside of the cylinder. =) woo or more vanes are receised into slots in the rotor and these are thrown out by centrefugal force when the notos notates =) The vanes move in and out of the slots in the notos and make effective contact with the cylinder. =) The whole assembly is kept submerged in an oil both inside the air tight casing. =) the vanes making the contact with cylinder divide the clearance space between rotos and cylindes into sections. =) The notation of the notor enables one of these to enpand in size while another is being compressed. =) Low pressure refrigerant vapour from evaporatos entors into the enpending section and gets compressed in the contacting section as the

notos notates I Compressed refrigerant vapour is forced out at high pressure into the condenser through the discharge value. =) These compressors are smaller in size and lighter in weight. These compressors have the advantage of being quiet in operation and reasonably free from vibrations Centrifugal Compressor Volute TIP Vany SAN gulet Impeller =) The centrifugal compressor increases the pressure of low pressure vapour refrigerants to a high pressure by Centrifugal force.

=) The centrifugal compressor is generally used for refrigerants that require large displacement and low condensing pressure, such as R-11 and R-113. I A single stage centrifugal compressor, in its simplest form, consists of an impeller to which a number of rived vones are fitted symm-- toucally 's =) The impeller rotates in an airtight volute casing with inlet and outlet points) The impeller draws in low pressure vapour refrigerant from the evaporatos. > when the impelles rotates, it pushes the vapour refrigerant from the centre of the impeller to its periphery by centrifugal force. =) The high speed of the impelled leaves the vapour referigerant at a high velocity at the wane tips

of the impeller. The kinetic energy thus attained at the impeller outlet is converted into pressure energy when the high velocity vapour refrigerant passes over the diffuser =) The diffuses is normally a vanders type as it permits more efficient part load operation which is quite usual in any air conditioning plant.) The volute casing collects the refrigerant from the diffuses and it purther converts the kinetic energy into pressure energy before the refrigerent leaves to the evaporator. Advantages of Centrifugal compressor over reciprocating compressors Dince the centrifugal compressors have no values, pistons, cylinders, connecting rod - the, therefore the

working life of these compressory is more as compared to reciprocating compressors. =) These compressors operate with little or no vibration as these are no inbalanced masses. I The operation of centerifugal > The centrifugal compressors run at high speeds (3000 R.P. Mand above) therefore these can be directly compared to reciprocating compressory I Because of the high speed, these compressors can handle large volume of vapour refergerant, as compared to recipiocating compressor. =) The centrifugal compressors are especially adapted for systems ranging from 50 to 5000 tonner They are also used for temperature ranges between -90°C to + 10°C =) The efficiency of these compresses is considerably high

=) The large size centrifugal compre--ssors require less floor area as compared to reciprocating compressors: Disadvantages =) The main disadvantage in centri-- fugal compressors is surging. It occurs when the reprigeration load decreases to below 35 % of the nated capacity and rauses severe stress conditions in the compressor.) The increase in poursive perstage is less as compared to recipro-- cating compressors. > The centrifugal compressors are not practical below SO tonnes rapacity load. The refrigerants used with these compressors should have high specific volume.

Condensers:

> The condenser is an important device used in the high pressure side of the refrigeration system. =) It's function is to remove heat of the hot vapour refrigerant discharged from the compressos Working of a Condenses Qual Brator Dischargeline Fre frigent Sinpansion value Suction Line J Receives 2 Jiquid frigerd Compressor. Sub-costing rejected & Condensation - H Desuperhest antermion Pressure Compression Evoporation, Enthalpy ->

=) First, the superheated vapour is cooled to saturation temperature corresponding to the pressure of the referigerant. This is shown by line 2-3. =) Now the saturated vapour refrigerant gives up its latent heat and is condensed ! to a saturated liquid refrigerant. this process is called condensation. It is shown by the line 3-4. =) The temperature of the liquid repri--gerant is reduced below it's saturation; temperature in order to increase the refrigeration effect. This is shown by the line 4-5. lypes of a Condensers According to condensing medium used, the condensers are classified into three groups. 1) Air Cooled condensers In these types of condensers, the theat removal is done by air.

- Tubing CIIII E Gulet CITITE Plate type fins outlet MITHING It is divided into two types :a) Natural convection. =) The heat transfer from the condenser coils to the air is done by natural convection and moentered force is applied 6) Forced convection =) It uses a fan to force the air over the condenser coils to morease it's heat transfer capacity. =) It is divided into two types :is) Base mounted air cooled condensers It uses fan which is mounted on the same base of the compressor, motor, receiver and other controly

(ii) Remote air cooled condensers These are used on systems above 10 tonner and are available upto 125 tonnes. The systems above 125 tonnes usually have two or more condenserse. These multiple condensers can be docated either inside or outside the building 2) Water cooled condensers. A water cooled condenser is one in which water is used as the condensing medium. These are classified into two types according to the type of water system they use:a) Waste water system Vapour refrigerant Hot vapour refrigerant water cooled condense compressos Water brown L Liquidrebrigerant Warmivotes to sever to receives

In this system, the water after conculating in the condenser is discharged to a server. b) Recipculated water system:-Vapour refrigerant Hot vapour prom evaporator == < Cooling $\leftarrow \mathbb{A} \leftarrow$ Cold water, Condenses water pund Compressor, Liquid refergerant to receiver. In this system, the same water is cooled again with a cooling tower or spray pond after getting discharged from the condenses and is used in the cycle again. According to construction the water rooled condensers are divided into three types :-

The second se

a) Tube in tube condenses :-Water out Not vapour reprigerant leee J $\rightarrow \rightarrow$ Waterin End Liquid refrigerant to receive =) This consists of a water tube mside a large reprigerant tube. In this type of condenser, the hot vapour referigerant enters at the top of the condenser. The water absorbs the heat from the refrigerant and the condensed liquid refrigerant flows. rat the bottom. > The cold water in the inner -tubes may flow in either direction.) when the water flows in the opposite direction of refrigerant ut is said to be counter-flow system.

I when the water flows in the same direction of the reforgerant it is said to be parallet flow system b) Shell and coil condensers:-Warm Coil water out Goil Shell Cold in . water in ---- Liquid reforgerant to =) A shell and coil condenser consists of one one more water coils ender in a welded steel shell. =) In this type of condenses, the hot vapour reprigerant enters at the stop of the shell and sworoundy the water coils. As the vapour. condenses, it drops to the bottom of the shell which often serves as a receiver.

c) Shell and tube condensers:-Babble Rebigeraint vapous condenses tuber The fit to condenses tuber tube sheet 5 II Water von cardense Jiquid ime =) The shell and tube condenser, consists of a colinderical steel shell containing a number of straight water tuby. =) the type tubes are enpanded into groover in the tube sheet holes to form a vapour-tight fit . The tube sheets are welded to the shell at both ends. I In this type of condenses, the hot vapour refrigerant entery at the top of the shell and condenses as it comes in contact with water tubes =) The condensed liquid refrigerant

drops to the bottom of the shell which often serves as a receives. 3) Evaporative condensers

do out 1112 + an Spray heades Spray heades Spray noggles Stot vo powr rufrigow A Cordenson Liquid refrigored cordenson Liquid refrigored sump A Make up wates

=) These condensers perform the combined functions of a water cooled condenses and a cooling tower. They use both air and water as a condensing medium. I In this operation, the water is pumped from the sump to a spray head and sprayed through noyles over the condenser coily

through which the hot vapour reforgerant from the compressor is passing . =) The heat triansfers from the refer--gerant through the condensing tabe walls and at the same time a fan draws ais from the bottom side of the condenser and discharged out at the top. > The air rauses the water from the surface of the condenser coils to evaporate and absorb the latent heat of evaporation from the remaining water to cool it. Comparision between water cooled and air cooled condensers Water cooled Air cooled i) Initial cost and maintenance cost is (i) Initial and main-- tenance cost both low are high . ii) These are no handling problems cii) these are difficult

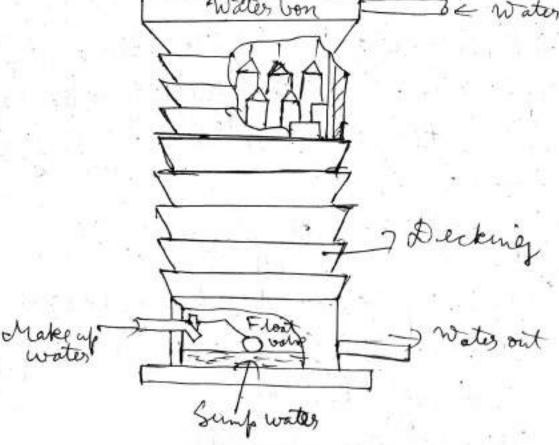
(iii) Pilpes are required ting they do not to carry water. require piping arrangement. civ) There are problem in disposing waste water. (iv) No problem in disposing (v) No fouling effect takes place (v) Fouling chances are very high (ii) High thornal (vi) Low thermal conductivity Conductivity (Vii) These are used (viii) These are used for for low capacity high capacity plants (VIII) Chere is no fan house (VIII) Fan noise uprese (ix) There is even (ix) The distribution distribution of water of ais on conden--ser surface is on the condensing surface. (x) These have (x) These have very high flenibility low flenibility

Heat Rejection factor The load on the condenser per unit of refrigeration capacity is known as heat rejection factor. Joadon Condenses (Qc) = Refrigeration Capacity + Workdone by compressor. $Q_c = R_E + W$. . Heat Rejection Factor $HRF = \frac{Q_{e}}{R_{E}} = \frac{R_{E} + W}{R_{E}}$ $= 1 + \frac{W}{R_E}$ $=1+\frac{1}{COP}$ Fouling Factor the water used in water - cooled condensers always. contain a Cortain amount of minerals and other foreign materials depending upon its source. The minerals form deposite inside the condenser water tubes. this is called water fouling.

Cooling Lower A cooling tower is an enclosed towes-like structure through which atmospheric air circulates to cool large quantities of warm Spray Ponds A spray bond conserts of a piping and spray nozice avrangement suspended over an outdoor open reservoir or pond. It can also cool large quantities of warm water. lypes of cooling towers 2) Natural draft cooling tower I In this the air circulates through The tower by natural convection I these are divided into two types:-() Spray type :-) The spray type cooling tower

consists of a bon shaped structure with Louvers . Speray header Sporay Worm water in noggles with the Worm condenses with condenses Make up De De Cooled water out to =) The lowers allow the atmospheric ais to pass through the tower, but slant down towards the inside of the towes to retain water in it. =) It should be located in an open space or on the roof of a building where the dis can blow freely through them (1) Splash deck type :-) The splash deck type cooling tower is similar to spray type cooling tower.) The water splashes on the decking from the holes in the bottom of a water bon on the top of a

Tower. > The object of decking is to increase the rate of heat transfer by enposing a large a mount of wetted surface to the air I The decking also helps to break up the water into small droplets and slows down the fall of water to the bottom of tower. Water, von Waterin



1 4 c 1 1 1

2) Mechanical draft cooling tower-The mechanical draft cooling towers are similar to at mospheric natural draft cooling towers encept the fans are used to force the ais through them. I These are divided into two types:-(2) Forced Draft :-In the forced draft cooling tower, a fan forces the air through the spray nozzles. =) The air is forced through the help of a propeller fan near the bottom of the tower. Air out 1711 climinatos Speray heades M M M M M M Spray nozzles Warm water in--an Fan motos 12 日老的山 Cooled water e out to condenses

-) The condenser worm water is cooled by means of evaporation. (i) Induced doraft Fan E tan Eliminator Spray header Worm water in The 252525 - Spray noysly forom condensos Louvery J. J WE winin whis in 31 Cooled water ========= < Make up water =) The induced draft cooling tower uses a fan to suck the air I these are similar to forced draft cooling towers except that The fors are located at the top instead of at the bottom and draw the air upword through the tower.

Evaporators =) The evaporator is an important device used in the low pressure side of a refrigerattion system. =) The referigerant boils in it by entracting heat from the surrounding Working of an Evaporator Liquid vapour minture Vapous, A refrigerant Ankansion value ine . 1 2 y Condenses Receiver - Liquid reprigerant Compressor =) The liquid reprigerant from the enpansion value enters into the evaporator coil at a temperature. below the temperature of evaporator

=) It enteracts heat from waponts and produce coldness. =) The products placed in evaporator, or fluids flowing through the reaporator coil are cooled. Classification of Evaporators 1) Bare tube Coil Waporatory Suctionline compressos == Empansion (..... Liquid D =) The bore tube coil evaporators are also known as prime-surface evaporators > It has a very simple construction hence it is easy to clean and deprost. =) It offers relatively lettele surface contact area which can be increased

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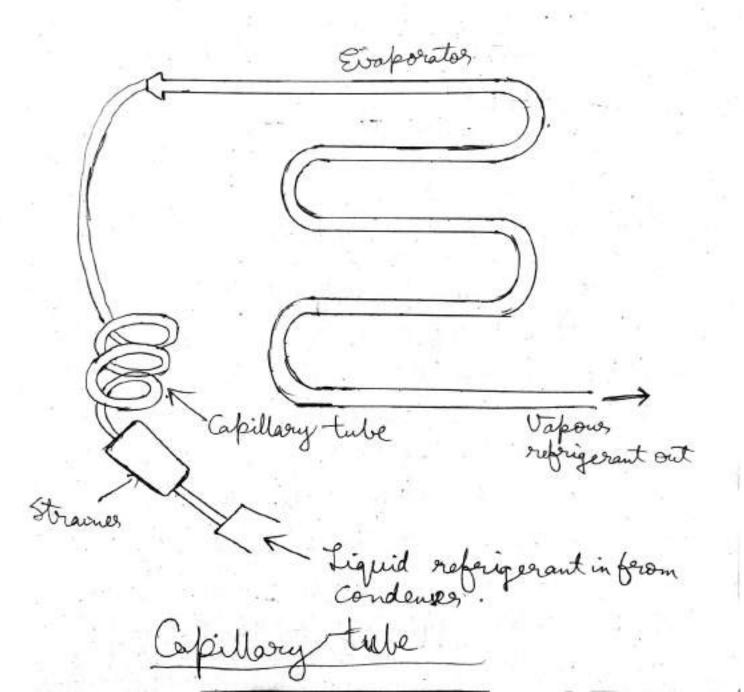
tube. These are limited to applications where the bon temperatures are under 0°C 2) Finned Evaporators Vapour reprigerant Finstill Jiguid ITTITT =) It consists of bare tubes or coils over which the metal plates or fins are fastened: =) The metal fins are constructed of thin sheets of metal having good thermal conductivity I Since the fins increase the contact surfaces for heat transfer, therefore the finned evaporators are also called entended surface waporators. These are designed for applications where, the temperature is above 0°C.

3) Shell and tube Evaporators Lequid in Chitled liquid out Vapar Refrigerant Reprigerant Jiquid Jiquid Thermostatic Bayles =) These are similar to shell and tube condensers. I These consists of a number of horizontal tubes enclosed in a cylinderical shell. The inlet and outlet headers with perforated metal tube sheets are connected at each end of the tubes. =) These evaporators are generally used to chill water or brine

Chapter-5 Reprigerant Flow Controls, Reprigerants and Application of Reprigerants Enpansion Valves :-=) The enpansion device is an important device that divides the high pressure side and the low pressure side of a refrigerating system. =). It is found between the condenser and the evaporator. renetion :-The enpansion device has the following functions:-⇒ It reduces the pressure of the reprigerant from high to low before being fed to the evaporator. > It controls the flow of refrigerant according to load on evaporatos.

It maintains the desired presso difference between the high and toro pressure rides of the system. Types of Expansion Devices is Capillary lube =) the capillary tibe is as an enfansion device in small capacity hermetic sealed refrigeration units =) It is a copper tube of small internal idiameter and of varying length dependending upon the application. =) The inside diameter of the tube used in reprigeration work is generally about 0.5 mm to 2:25 mm and the length varies from D. Sm to Sm. =) A small filter driver is used on some systems to provide additional preeze -up application =) The refrigeration system using "apillary tube the following advantages. 1) It's cost is less than other

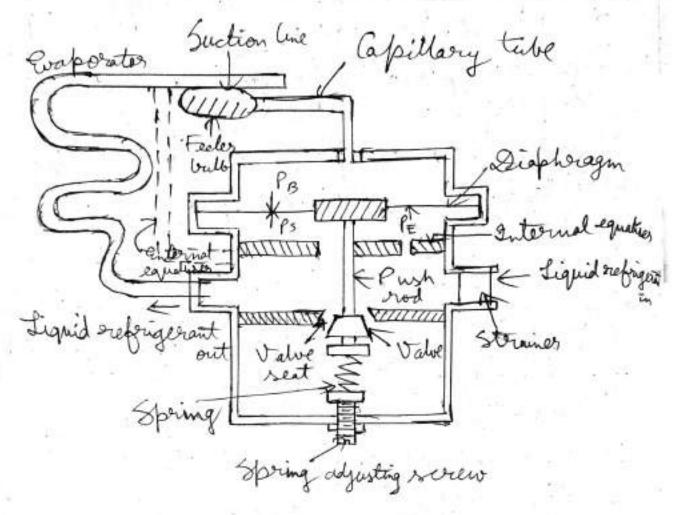
enpansion devices. 2) The refrigerant charge is critical, therefore no receives is necessary. 3) The refrigerant continues to blow into the evoporator and equalises the pressure even after the compressor stops therefore the load and the Compression is reduced.



(i) Automatic Enpansion Value Diafhrogen prening Rusp. pressure refrigerant out to evoporate, Strainer Falve Liquid - ----=) the automatic enpansion value is also known as constant pressure enpansion valvebecause it maintains constant evapor -rator pressure regardless of the load on the evaporator. =) The automatic enpansion value, consists of a needle value and a seat, a metallic diophragen or bellows, spring and an adjusting screw. =) The opening and closing of the when two opposing forces acting on

the disphragm: 2) The spring pressure and atmospheric pressure on top of the diaphragen 2) The evaporator pressure acting below the diaphragen Then the compressor is running, the value maintains an evaporator pressure in equili-- brium with the spring pressure and the atmospheric pressure. => Any increase in evoporator pressure (perps) pushes the diaphragm up, causing the value to move in closing direction and admit less refrigerant. > Any decrease in evaporatos pressure (pe<p) results in the movement of diaphragm downwards , so that the value opens more and admits more refrigerant. =) At correct spring retting (Ps=Pe), the amount of fluid flowing through the value enactly valances the compressor pumping capacity at designed suction pressure.

(iii) Thermostatic expansion value



=) The thermostatic enfansion value, consist of a needle value and a seat, a metallic diagbragen, spring and on adjusting screw.

In addition to this jet has a feeles of thermal bullo which is mounted on the suction line near the outlet of the evalporator coil. It is partially filled with the same liquid refrigerant as used in the refrigeration system.

=) Any change in temperature of the refrigerant will cause a change in pressure in the feeler bull which will be communicated to the top of diaphragm. I The evaporator pressure and spring force act beneath the diaphragm in closing direction of the value whereas pressure enerted by power fluid above the diaphragm'acts in the opening direction =) Any increase in heat load or decrease in refrigerant will increase the superheat and the pressure on the top of the diaphragm, moving it to open the value to a closed position. =) Under normal operating conditions the value achieves a valanced condition (Po = Ps+Pe) where the refrigerant flow balances the heat load. =) Thermostatic empansion value is most suitable for comparatively high evapor-- atos temperature operation and is the mostly used form of enpansion device in air conditioning and reprigeration systems.

=)The thermostatic enpansion value serves the following functions:-(1) to reduce the pressure of the liquid reprigerant from the condenser pressure to evaporatos pressure - Throttling action. (1) To allow the flow of liquid refrigerant to the evaporator according to load requirements of the evaporator so as to prevent the starving of evaporator or flooding the compressor. Reprigerants The refrigerant is a heat carrying medium which dwing their cycle in the reprigeration system absorbs heat from a low temperature system and discards the heat so absorbed to a higher temperature system.

Classification of Refrigerants The refrigerants are mainly classified into two groups:-1) Primary refrigerants. 2) Secondary reprigerants. -) The & reprigerants which directly take part in the reprigeration system are called primary reprigerants. =) The referigerants which are first cooled by primary refrigerants and then used for cooling purposes are known as secondary refrigerants The primary reprigerants are further classified into four groups:-(i) Halo- carbon or organic =) This group contains refrigerants having one or more of three halogens (chlorine, bluorine, bronnine)

=) These are all synthetically peroduced and are available in the market under trade names of Freon, Genetion Isotion and Aretron. =) Few enamples of Halos carbons are R-11, R-12, R-13, R-134a-ete (ii) Azeotrope) Azeotrope is a stable minture of referigerants whose vapour and liquid phases retain identical compo--sitions over a wide range of temperatury I Some common Azeobiopes are R-500, R-502, R-503, R-504. (iii) Inorganic Reprigerents =) Inorganic compounds were used - corbon reprigerents and are the oldest form of refrigerants. =) They possess excellent properties but are highly tonic and flammable.

) Some enamples of Inorganic compounds are R-717 (Annonia), R-729(dis), R-744(CO,), R-764&-etc (iv) Hydro- Carbons =) Hydrocarbon refrigerants are used in low temperature applications and are made from carbon and hudses hydrogen. =) They are highly flammable and explosive but possess satisfactory tiermodynamic properties -> Their use are limited to chemical and refining industries only.) Some enamples of hydrocarbons are R-170(Ethane), R-290 (Propane), R-600 (Bestane), R-600 a (Isoloutane), R-11 20 - etc.

Secondary Reprigerants ⇒ Water and Brines are widely used of secondary referigerants. Wates I water is used as a refrigerant where the temperature is to be maintained above the preezing point of water i e 0° c. The water is first cooled by a primary reprigerant and is then allowed to be circulated through the tubes by means of a pump. Brine =) These are used as a secondary refrigerant where the temperature to be maintained is below the precising point of water such as in on ice plant. =) It is a solution of salt in water because addition of salt in water reduces the preesing temperature of water solution than that of =) En:- Na cl, Call2-etc.

Desirable properties of an Edeal Reprigerant 1) Low boiling and preezing point 2) High critical pressure and temperature. 3) High latent heat of vaporisation. 4) Joio specific heat of liquid and high specific heat of vapour. 5) Jow specific volume of vapour. 6) High thermal conductivity 7) Non-corroswe to metal 8) Non-flammable and non-enplosive 9) Non-tonic 10) Low cost. 12) Easy to liquify at moderate pressure 3) Easy of locating leaks by odour 14) Mines well with oil. 15) Aigh co-efficient of performance 16) Ozone friendly.

Designation of Reprigerant =) The refrigerants are internationally designed as 'R' followed by certain mumbers. numbers =) A refrigerant followed by a two digit number indicates that a refrigerant is derived from methane base while three - digit number represents ethane base. = The first digit on the right is the number of fluorine (F) atoms , second digit is hydrogen (H) atoms + 2, and the third digit is number of corbon () atomi - 1. =) when the number of rarbon atoms is zero it is omitted. > The general chemical formula for the refrigerant, either for methan or ethane base is given by CmHh Up Fg in which The total = 2m + 2Fwhere m = No of carbon atoms n= No of hydrogen atoms p= No of chlorine atoms q = Wo of fluorine atoms.

=) The number of refrigerant is given by R(m-1) (n+1) ?! 1) Dichloro-difluoro-methane No of chlorine atoms, p = 2 No of fluorine atoms, q = 2 No hydrogen atoms, n=0 n+p+q=2m+2= 20+2+2=2m+2=) m=1 No of Carbon atoms = 1 Chemical Formula = CCL2F2 No of Refrigerant = R(m-1)(n+1)q = R(1-1)(0+2)2 7) R-12 2) Dichloro - teterfluoro ethane p = 2, q = 9, n = 0 $nt_ptq_1 = 2m+2$ 0 + 2 + 4 = 2m + 2=) m=2 Chemical formula = C2 C12 Fy Wo of refrigerant = R(2-1) (0+1) 4

3) Dichloro-trifluoro= ethane p=2, q=3, n=1 n+p+q=2m+21+2+3=2m+2 =) m=2 Chemical formula = C2 H C12@F3 No of refrigerant = R(2-2) (1+2) 3 =) R-123 4) <u>R-22</u> R(m-1) (n+1)p -) Refe m-1=0 =) m=2 n+1=2 =) ~=1 .p=2 (n+p+q)=2m+2(1+2+q) = 2x 1+2=) q/=1 Therefore chemical formula = CIFCL F2 (Monochloro diffuorometting)

5) R-114 R(m-1)(n+1)pm - 1 = 1=) m = 2· n+1=1 =) n = 0 JP = 4 (n+p+q)=2m+2=)(0+4+q)=2x2+2=) q/=2 Therefore, C2 (12 Fy ethane Dichloro-tetrafluoro Thermodynamic Properties of Reprigerants 1) Boiling temperature :-=) The boiling temperature of the reprigerant at atmospheric pressure should be low. > If the boiling temperature of refei--gerant is high at atmospheric pressure, the compressor should operate at high vacuum =) The high boiling temperature reduces the capacity and operating cost of system.

2) Foreezing temperature :-=) the precying temperature of a refrigoal . Should be well below the operating evaporatos temperature =) It is below - 35°C in most of the reprigerants . 3) Evaporator and condenser pressure: > Both the pressures should be positive and be as near to the atmospheric pressure as possible in order to prevent leakage of air and moisture into the refriger - ating system. =) loo high evaporating and condensing pressures would require stronger refrigerating equipment resulting in higher initial cost. 4) Gritical temperature and pressure:-=) The critical temperature of a refri-gerant is the highest temperature at which it can be condensed to a liquid regardless of a higher pression

=) It should be above the highest Condensing temperature that might be encountered or else encessive power consumption results 5) Co-efficient of performance and power requirements =) For a ideal reprigerant operating between - 15°C evaporator temperature and 30°C condenser temperature, the theoretical co-efficient of performance for the reversed Carnot cycle is 5.74. =) Practically, all common refeigerants have approximately the same coeffi--cient of performance and power requirement. 6) Latent heat of vaporisation =) A refrigerant should have a high latent heat of vaporisation at the evaporator temperature.) The high latent heat results in high referigerating effect per

Ag of refrigerant conculated which reduces the mass of refrigery to be circulated per tonne of refrigeration. 7) Specific Volume I the specific voleime of the refrigerant Vapour at evaporatos temperature indicates the theoretical displacement of the compressor. =) The reciprocating compressors are used with refrigerants having high preisures and low volumes of suction Vapour. > The centrifugal compressors are used with refrigerants having low -pressures and high volumes of suction vapour. =) The notary compressors are used with reprigerants having intermediate pressures and volumes of the suction vapour.

Chemical properties of Refrigerants 1) Flammability :-=) It is the ability of a refrigerant to catch fire with ease. =) Hydro carbon refrigerants are highly flammable and Ammonia Acomes enplosive when mined with air the ratio of 16 to 25%. =) The halo-carbon reprigerants are neither flammable nor enplosive. 2) Tonicity :-⇒ Tonicity is the property of a refrigerant to be poisonous or harmful towards atmosphere. =) It may be of primary or secondary importance depending on the application =) Some non-tonic reforgerants becomestonic when mined with Certain percentage of air

3) Solubility of water - Reprigorant should be soluble in wates at right amount or else ice may form which chokes the enpansion value I this may be avoided by proper delightation of the reforgeerating unit before charging 4) Miscibility =) The ability of a reprigerant to min with oil is called mocibility. -) The freen group of reprigerants are highly missible while morganie reprigerants are non-miscible. =) The non-miscible reprigerants require larger heat transfer conduction properties of oil.

5) Effect on perishable materials =) The reprigerants used in cold storage plant and in domestic reprigerators should be such that in case of leakage, it should have no effect on the perishable materials. =) Freen group of refrigerants have vegetably and furs. Products, mests =) Methyl chloride vapours have no effect upon furs, plowers, eating foods or derinking beverages. =) Ammonia dissolves easily in water and becomes alkaline in nature therefore it reacts with products that areacidic in nature

1.1

Commonly used Reprigerants 1) <u>R-11</u> (Trichloro-monofluore methane (CC457) It is a synthetic chemical powder which can be used as a refeigerant. =) It is stable, non-flammable and non-tonic and is a low presserie refrigerant. =) It has a low side pressure of 0.202ba, at - 15°C and high side pressure of 1-2606 bar at 30°C =) The latent heat is 195 KJ/kg at -15°C and the boiling point is 23.77° c at Atmospheric pressure. =) It is used for large contribugal compressory of 200 TR and above : 2) <u>R-12</u> (Dichloro difluoro methane) (CC/2F2) =) It is a colourless, odourless, non-tonic, non-corrosive, non-irritating and non-flammable reforigerant =) It has a boiling point of -29°C at atmospheric pressure =) It has a pressure of 0.82 bas at 15°C and a pressure of 6.4 bas at 15°C

30°C . =) It has a latent heat of 159/KJ/kg at 15°C =) It is used in referigerators, freezers, water coolers, room and window air -- conditioning units - etc 3) R-22 (Monochloro-difluoro-methane) (CHICLES) =) It is a synthetic refrigerant used for fast preezing units which maintain a temperature of -29°C to -40°C. =) Its boiling point is -41°c at atmospheric pressure and has a latent heat of 216.5KJ/kg at-15c. =) The normal head pressure of R-22 at 30°C is 10.88 bar and the evapor-- atos pressure is 1.92 bar at -15°C =) The refrigerant is stable and is non-tonic, non-corresive non-iovitating and non-flammable. I It is used in reciprocating and centrifugal compressors and has also been successfully used in air - conditioning cenity in household reprigerators.

4) R-134a (Tetrafluoro ethane) (CF3CH2F) =) It is considered as the most preferred substitute for reprigerant R-12. =) It has a boiling point of -2.6.15°C. =) It has no chlorine atom therefore this refrigerant has sero ozone depleting potential (ODP) and has 74 % less global warming potential Compared to R-12. =) Since the molecules of R-134a are smaller therefore a very sensitive leak detector is used to detect leaks. =) It is now-a-days widely used in Car-air-conditioners 5) <u>R-717</u> (Ammonica) (NH3) I'It is one of the oldest and most widely used of all refrigerants. =)"It is a colourless gas and is tonic, flammable and enplosive in nature. =) It's boiling point is -33.3°C and melting point is - 78°C.

) It's latent heat of vaporisation is at -15°C which is 1315 KJ/kg. =) The condenser pressure for R-717 is 10.78 bar at 30°C. =) The condensers for R=717 areusually of water coold type. =) It's greatest application is found in large and commercial reciprocating compression systems where high tonicity is secondary Jubstitute for CFC > the Chloro Fluoro carbon (CFC) refrigerants have been linked to the depletion of oyone layer and have a global warming effect. =) Due to this reason certain substitutes are being looked for to suplace CFCs. =) Two of the chemical classes under consideration for replacing (FCs are

hydrochlorofluorocarbons (H(FG). and hydro-fluoro-carbons (HEFG). =) HCFCscontribute to ozone depletion but to a much lesser entent than CITCS.

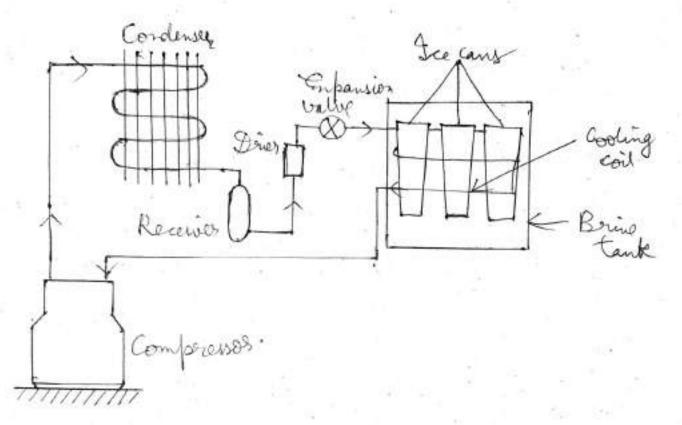
- =) Therefore HFCs have lowest oyone depletion potential in addition to loss global warming potential =) it present the following substitutes are available :-
 - 1) $R 123 (CF_3(H(1_2)) for R 11(C(1_3F))$ 2) $R - 134a (CF_3(H_2F)) and R - 152a (CH_3(HF_2))$ for R - 12.
 - 3) R-143a (CH3CF3) and R-125(CHIF2CF3) for R-502.
 - 4) R-290 ((3H8) and R-600a (C4H10) as an additional substitute for R-12.

Applications of Reprigeration Certain applications of reprizonation (i) Cold Storage I It is a space designed to store -perishable food stuff within well depined temperature and humidity. =) It is used to preserve fish meat, builts , vegetables and medicines . -V-V-V-Refrigerated WW-W-Blower Condenser With How Blowers Condenser With Receiver & With Receiver & Staposator coil - Compresson ATTT It works on vapour compression system. # It prevents the spoilage of perishable commodities and make them available in all the seasons and in places where they are not howester.

(i) Davy reprigeration ⇒ Milk and dairy products are very essential for human nutrition and development and has a very increasing demand woorldwide . =) Although it is a highly nowishing 600d, haw fresh milk is highly liable to not and can easily spoiled by the growth of micro-organisms. =) Therefore a reprizeration system is used for processing of milk. =) and to keep it preserved until it is delivered (ii) Ice plant =) See is produced artificially from clean water by chilling " Ice making plant consists of a vapour compression system with Ammonia as a refrigerant. If also uses brine to prevent

heat transfer from swowending to it

=) The ice produced through it is widely used to chill cold drinks, or transport daivy products or perishable commotities such as fishes, femity - etc.



civ)Wates cooles > The purpose of a water cooler is to make cold water available at a constant temperature irrespective of the ambient temperature) They are meant to produce coldwates at about 7°C to 13°C (280 K to 286 K) for quenching the thirt of people.

=) Water coolers are classified as (i) Storage type (ii) Instantaneous type. =) In a storage type water cooler, a cooling coil is writeped around the water storage tank and cold water is available in the tank at all times. > In an instantancous cooles, cooling coil is weaked around the pipe line. Water is cooled to the desired temperature by the time it reaches the tank. (v) trost tree refrigerator =) A Frost Free refrigerator offers an even distribution of cool ais within the refrigerator by means of electric frans. =) Since this technology prevents the formation of ice, no deposting is necessary.

PSYCHROMETRY AND PROPERTIES CHAPTER - 6

-> In this psychrometry chapter the properties of mindure of airc and walen vapour are studied.

Dry Air - The dry air is comidenced as a minture of netrogen and onygen reglecting the small percentages of

Moist Ain: - It is a minimume of along aire and water vapour

water vapours - The water vapour present in air is known as moisture

Dry Bull Temperature: The temperature of air measured by ordinary thermometers is known as dry bull temperature (DBT).

Wet Bulb Temperature - The temperature measured by the theromometers when its bulb is covered with wet cloth and is exposed to a current of moving airs is cloth and is exposed to a current of moving airs is known as wet bulb temperature. The differences between por and WBT is known as WBD.

Der point temperature: - The temperature of the air in reduced by contineous cooling then the crater vapour in the cure will start condensing out a particular temperature. The temperatures at which the condensing starts in known as deer point temperature DPT in the starts in known as deer point temperature DPT in the starts is known as deer point temperature DPT in the starts of known as deer point temperature DPT in the

specific humidity - It is the man of water vapour . present per 15g of dry air

Absolute humidity: - The weight of water vapour present in unit volume of aire is known as absolute humidity.

degnée of saturation : - The degree of saturation is defined as the natio of man of water vapour associated with unit man of dry ain to man of associated with unit man of dry ain to man of dry ai water vapour anociated with unit man of dry ai secturaled at the same temperature.

Relative Humidity !- The relative humidity is defined as the ratio of actual mays of water vapour in a given volume to the mass of water vapour is the air is saturated at the same tempera

* Dalton's Law of partial pressure

94 states that the total pressure of a minter of gases is equal to the sum of the partial pressures enerted by each gas.

T mineure of	(a)	Gas (b)	Gas (c)
gaves a,	The second	1	0 00000

As per Dalton's law of partial pressure

 $\int P_t = P_a + P_b + P_c$

gf this law is appliered to the moist air which contains dry air and waler vapour, then Pt=PatPv

Pt = Total pressure of moist air pa = partial pressure of dry air pr = partial pressure of arater vapour.

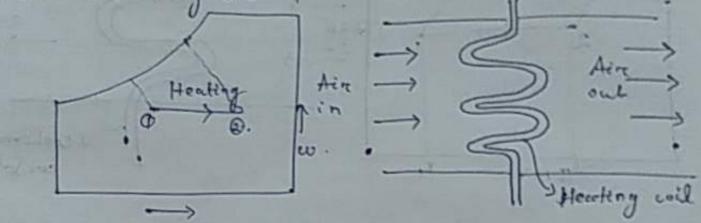
Specific Humidity :-It is the mass of water vapeurs present per kg of dry air. w= mais of water vapour in mixture mean of drey cuire in minture $\omega = \frac{m_v}{m_a}$ $\omega = \frac{\left(\frac{P_v V}{R_v T}\right)}{\left(\frac{P_a V}{R_v T}\right)} = \frac{P_v V}{R_v T} \times \frac{R_a T}{P_a v} = \left(\frac{R_a}{R_v}\right) \times \left(\frac{P_v}{P_a}\right)$ 1 - 1 - 1 - $Ra = \frac{K}{Ma}$, $R_v = \frac{K}{Mv}$ $cv = \left(\frac{K_{ma}}{K_{m}}\right) \times \frac{Pv}{Pa}$ $=\left(\frac{M_v}{M_a}\right) \times \left(\frac{P_v}{P_a}\right)$ $=\left(\frac{18}{29}\right)\times\left(\frac{Pv}{Pa}\right)$ $\omega = 0.622 \times \left(\frac{P_V}{P_L - P_V}\right)$ Relative Humidity: (1) -: $\phi = \frac{mars of water vapour in a given volume }{mars of water vapour in same volume if saturate$ $= \frac{mv}{mvs} = \frac{\left(\frac{PvV}{RvT}\right)}{\frac{PvV}{Pvs}} = \left(\frac{Pv}{Pvs}\right).$ (PUV) BUT $\phi = -\frac{Pv}{Pvs}$ Scanned By CamNScan

Degree of Saturation
$$(\mu):-$$

 $\mu = \frac{main of water vapour associated with unit more at dry air
mass at water vapour associated with saturated with mass of dry air.
 $\int \mu = \frac{\omega}{\omega_{3}}$
 $\mu = \frac{0.622(\frac{h}{P_{1} - P_{2}})}{0.62(\frac{P_{2}}{P_{1} - P_{2}})}$
 $\int \mu = \frac{P_{2}(P_{1} - P_{2})}{P_{2}(P_{1} - P_{2})}$$

PSYCHROMETRIC PROCESS :-

O Sensible Heating :- Heating of air without addition of moisture is termed as sensible heating. -> The heating can be achieved by passing the aire over the heating coil .



-> In this process the drybult Temperature (DBT) increases specific humidity rumains constant. -> enthalpy value in this process increases and wet built temperature increases. -> Relative humidity value decreases in this -> Relative humidity value

iensible cooling Ain coolir TADBT Tel

→ Cooling of air cuithout rejecting the moisture from the own is termed ou' représente cooling.
→ This process à represente in the psychrometrie chart by the line (1-2) from reight to left.
> The heat rejected by our alaring semible cooling may be obtained from the psychrometrie chart by the enthalpy difference (h₁-h₂).
→ 9n this servible cooling process the specific humidity remains constant.

-> The daybulb temperature reduces from top ato top > The relative humidity value increases from \$\overline to \$2.

-> heat rejented can be calculated by using the following formula.

 $q = h_1 - h_2$

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CCAT

-> Ain enters at condition 1 and leaves at
condition 2.
-> In this process both day bulb temperature
and specific humidity increases.
> The final relative humidity of the ain
can be highen on lower than that of the
entering ain.
Total heat added

$$q = h_2 - h_1$$

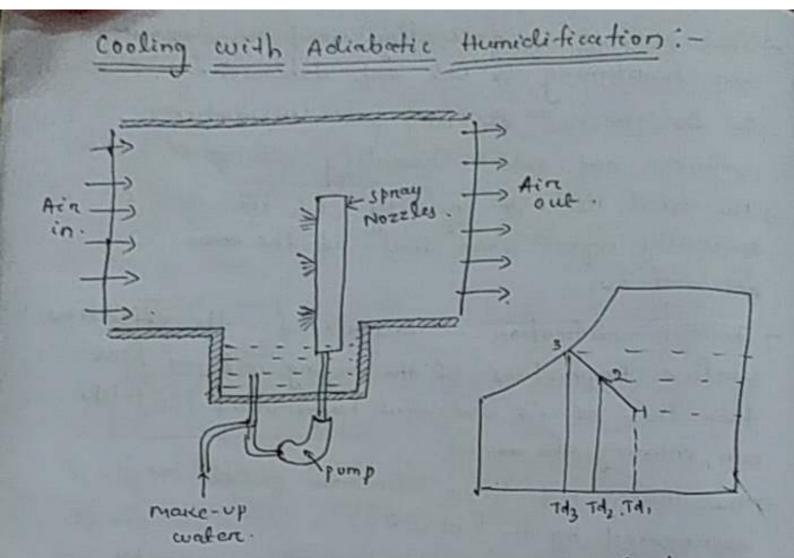
 $\int q = (h_2 - h_3) + (h_3 - h_1)$
 $h_2 - h_3 = Latent heat of vapource sectors
 $h_3 - h_1 = sensible heat added$.
Cooling and Dehumidification
 h_2
 h_3
 $h_2 - h_3$
 $h_3 = bot - h_1$
 $\int q = (h_2 - h_3) + (h_3 - h_1)$
 $h_2 - h_3 = Latent heat of vapource sectors
 $h_3 - h_1 = sensible heat added$.
 $for h_3$
 $h_2 - h_3 = bot - h_1$
 $for h_3$
 $h_3 - h_1 = sensible heat added.
 $for h_3$
 $h_3 - h_1 = sensible heat added.
 $for h_3$
 $h_3 - h_1 = sensible heat added.
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 $h_3 - h_1 = sensible heat added.
 $for h_3$
 $h_3 - h_1 = sensible heat added.
 $for h_3$
 $h_3 - h_1 = sensible heat added.
 $for h_3$
 $h_3 - h_3 = bot - h_3$$$$$$$$$

->This process is generally used in summer cuire conditioning to cool and dehumichity the ->In this process the dray bulb temperatures reduces and specific humidity decreases ->The final relative humidity of the cure is generally higher than that of the cure. entering aire.

> The dehumidification is possible if the effective runface temperature of the cooling coil is less than that of the clew point temperature of the cuir entering the coor coil.

> The wolling and dohumillification process is represented by the line (1-2).

 $\rightarrow \text{The total removed in the present is given by}$ $Q = (h_1 - h_2) = (h_1 - h_3) + (h_3 - h_2),$ Q = (LH) + SH



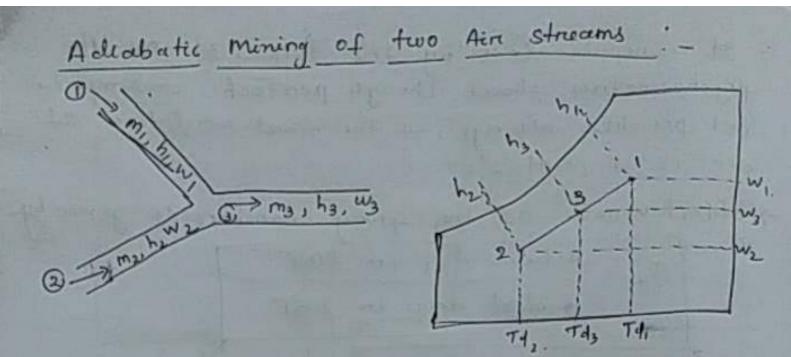
→ when the air is passed through an imulated chamber, having Sprays of water maintained at a temperature (t1) higher than the dew point temperature of the entering ein (tdp1), but lower than its chy bulk temperature (td1) of entering air. → The temperature of the spray water is equal to the wet bulk temperature applied and humiclified. Since no heat is supplied on rejected from the spray water, so the adiabatic suburation happens . In this process wet bulk temperature premaine constant. -> It is represented by the line (1-3) on the psychnometric chart. Though perfect cooling is not possible always, so the final condition of air is at point 'D'. -> effectiveness of the spray chamber is given by $2\mu = \frac{Actual}{Actual} drop in DBT$

 $= \begin{array}{c} T_{d_1} - T_{d_2} \\ T_{d_1} - T_{d_3} \end{array}$

alue it can be represented by the modifferer between the specific humidity.

NETTING & PROPERTY

 $\mathcal{Q}_{H} = \frac{\omega_{1} - \omega_{2}}{\omega_{1} - \omega_{3}}$



Consider two air streams () and () mining adiabatically as shown in the above figure. $m_1 = mass$ of air entering at () $h_1 = mass$ of air entering at () $h_1 = enthalpy$ of air entering at () $w_1 = specific$ humidity of air entering at (). $w_1 = specific$ humidity of air entering at (). $m_2, h_2, w_2 = mass, enthalpy and specific humidity of$ air which are entering at point (). $<math>m_3, h_3, w_3 = mass, onthalpy and specific humidity of$ air at point ().

$$\rightarrow For mass balance \xrightarrow{m_1 \leftrightarrow p} (m_1 + m_2 = m_3) \longrightarrow \mathbb{O}$$

$$\rightarrow For onerrow balance \xrightarrow{m_1h_1 + m_2h_2 = m_3h_3} \longrightarrow \mathbb{O}$$

For mass balance of water vapour

$$\begin{bmatrix} m_1w_1 + m_2w_2 &= m_3 & W_3 \\ \hline m_1w_1 + m_2w_2 &= m_3 & W_3 \\ \hline m_1h_1 + m_2h_2 &= m_3h_3 \\ = \end{pmatrix} m_1h_1 + m_2h_2 = (m_1 + m_2)h_3 \\ = \end{pmatrix} m_1h_1 + m_2h_2 = m_1h_3 + m_2h_3 \\ = \end{pmatrix} m_1(h_1 - h_3) = m_2(h_3 - h_2) \\ =) \begin{bmatrix} \overline{m_1} &= h_3 - h_2 \\ \overline{m_2} &= h_3 - h_2 \\ \overline{h_1 - h_3} \\ \end{bmatrix}$$
Now substituting the value of m_3 in eq⁷ (5)
 $m_1w_1 + m_2w_2 = m_3 & W_3 \\ \Rightarrow m_1w_1 + m_2w_2 = m_1w_3 + m_2w_3 \\ \Rightarrow m_1w_1 + m_2w_2 = m_1w_3 + m_2w_3 \\ \Rightarrow m_1w_1 + m_2w_2 = m_1(w_3 - w_3) \\ \end{cases}$

$$\Rightarrow m_{1}w_{1} + m_{2}w_{2} = (m_{1}+m_{2})w_{3}$$

$$\Rightarrow m_{1}w_{1} + m_{2}w_{2} = m_{1}w_{3} + m_{2}w_{3}$$

$$\Rightarrow m_{1}(w_{1} - w_{3}) = m_{2}(w_{3} - w_{2})$$

$$\Rightarrow \boxed{\frac{m_{1}}{m_{2}}} = \frac{w_{3} - w_{2}}{w_{1} - w_{3}}$$

$$So \left[\frac{m_{1}}{m_{2}} = \frac{h_{3} - h_{2}}{h_{1} - h_{3}} = \frac{W_{3} - W_{2}}{W_{1} - W_{3}} \right]$$

Catalogue 1. Marshell Daniel & Provinsi Human Combort -ीत एक जिल्हा म It is that condition of mind which expresses with the enviormment (cold or hot). The human body works best at a certain

Ettective temperature, -The degree of warmth or cold (temperature) felt by human body depends mainly on the bollowing

fluree bactors : a. Dry bulb temp. 5. Relative humidity 3. Air velocity.

- -> Ebbertive temperature is debind as that index which corelates the combined ebberts of dry bulbtimp; relative humidity and air velocity on the human body.
- -> The value of effective temp. is equal to the temperature of still saturated air (i.e 5 to 8 m/min air velocity)
- > # The practical application of eldertive temp is presented by Combort Chart.

Faitors abbrecting Optimum Etherhie temperature

→ The people living in colder climates
→ The people living in colder climates
teel combortable at a lower timp.
than those having in warmer region.
> In winter season the optimum
ebbechive temp. is 19°C and
in summer season the optimum
ebbechive temp. is 22°C.

(2) (lothing : -> The penson with light clothings need less optimum temperature than a person with heavy clothings. 3 Age and Sere : -> The women of all ages require higher elstrective temp. (0.5°c) than nen. > The children also need higher ebbective temporature than adults. (4) Duration of stay --) the stay in a room is (i. einbank) shorter, then effective temp. is required higher than bor long stay (i.e in attrice) (5) hind of activity -I when the activity of person is theavy such as the people woshing in a bartony dancing hall then low elbechive temp. is needed than bor the people sitting in a cinema hall. Density of Occupants: I The effect of body radiant heat brom person to person in advantitionium is large which require a slight lower effective temperature.

Combort chart :

-> A chart which relates elsertive temp, dry bulls temp, wet bullstemp. and air movement to human combort -> In this chart, the dry bulls temp is taken as abscirsa and the wet bulls temperature as ordinates.

-) The study of the chart reveals that the several combinations of wet and dry bulls temperatures with different relative humidities will produce the same effective temperature.

-> The combort chart shows the range bor both summer and winter condition when within which a condition of combort enists for people.

→ For winter condition the combort chart indicates an ebbeitive temp. of 20°C. It bor 97.7.1. people and bor Summer condition

the combort chart indicates on elbertie temp: dr 21:6°C drags bor 984. people. > for combort condition the women requir 0.5°C higher elbertive temp. than men > The greater the degree of activity.

the lower the ebbective temp. necessary

I the elbertive temp. is 21°C for still air velocity i.e 6 m/min at 24°C obry bulls temp. and 16°C wet bulls temp. condition.

CHAPTER -7

AIR CONDITIONING SYSTEMS

Air conditioning is the process of removing heat and moisture from the interior of an occupied space to improve the comfort of occupants. Air conditioning can be used in both domestic and commercial environments. This process is most commonly used to achieve a more comfortable interior environment, typically for humans

Factors affecting comfort air conditioning:

Following are the Factors affecting Comfort Air conditioning:

- 1. Temperature
- 2. Humidity
- 3. Purity of air
- 4. Motion of air.

Temperature of air. In air conditioning, the control of temperature means the
maintenance of any desired temperature within an enclosed space even though the temperature of
the outside air is above or below the desired room temperature. This is accomplished either by the
addition or removal of heat from the enclosed space as and when demanded. It may be noted that
a human being feels comfortable when the air is at 21°C with 56% relative humidity.

2. Humidity of air. The control of humidity of air means the decreasing or increasing of moisture contents of air during summer or winter respectively in order to produce comfortable and healthy conditions. The control of humidity is not only necessary for human comfort but it also increases the efficiency of the workers. In general, for summer air conditioning, the relative humidity should not be less than 60% whereas for winter air conditioning it should not be more than 40%.

3. Purity of air. It is an important factor for the comfort of a human body. It has been noticed that people do not feel comfortable when breathing contaminated air, even if it is within acceptable temperature and humidity ranges. It is thus obvious that proper filtration, cleaning and purification of air is essential to keep it free from dust and other impurities.

4. Motion of air. The motion or circulation of air is another important factor which should be controlled, in order to keep constant temperature throughout "the conditioned space. It is, therefore, necessary that there should be equi-distribution of air throughout the space to be air conditioned.

Equipments Used in an Air Conditioning System

Following are the main equipments or parts used in an air conditioning system :

1. Circulation fan. The main function of this fan is to move air to and from the room.

 Air conditioning unit. It is a unit which consists of cooling and dehumidifying processes for summer air conditioning or heating and humidification processes for winter air conditioning.

 Supply duct. It directs the conditioned air from the circulating fan to the space to be air conditioned at proper point.

4. Supply outlets. These are grills which distribute the conditioned air evenly in the room.

 Return outlets. These are the openings in a room surface which allow the room air to enter the return duct.

 Filters. The main function of the filters is to remove dust, dirt and other harmful bacteria from the air.

Classification of Air Conditioning Systems

The air conditioning systems may be broadly classified as follows :

1. According to the purpose

(a) Comfort air conditioning system, and

(b) Industrial air conditioning system.

2. According to season of the year

(a) Winter air conditioning system,

(b) Summer air conditioning system, and

(c) Year-round air conditioning system.

3. According to the arrangement of equipment

(a) Unitary air conditioning system, and

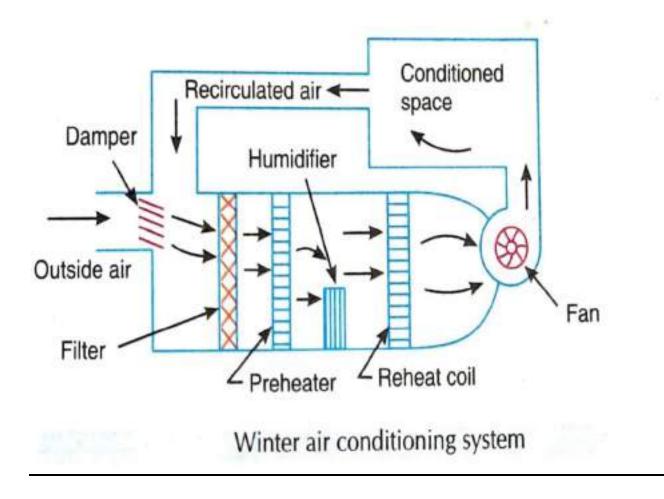
(b) Central air conditioning system.

Winter Air Conditioning System:

In winter AC System, the inlet is heated by the heater, and in winter season due to less present in the air, we also need to add the moisture particle to the air, generally, a humidification system is added to maintain the moisture quantity.

Working of Winter Air Conditioning System:

In winter air conditioning, the air is heated and is accompanied by humidification.



1. The outside air flows through a damper and mixes up with the recirculated air which is obtained from the conditioned space.

2. The mixture here passes through a filter to remove dirt, dust, and other impurities.

3. The air now passes through a preheat coil to prevent possible freezing of water due to which dry bulb temperature increases to a very high value and the relative humidity drops to a low value.

4. This air is being pumped into the humidifier.

So, humidification of air (addition of moisture) is done and then the air is made to pass through a reheat coil to bring the air to the designed dry bulb temperature.

5. Now the conditioned air is supplied to the conditioned space by mea fan. From the conditioned space, a part of the used air is exhausted to the atmosphere by the exhaust fans or ventilators.

The remaining part of the air known as recirculated air is again conditioned

6. Initially, the relative humidity is 60% in the winter season, so to reduce it, a process of reheating is done where it is reduced to 20%.

So it is again humidified due to which it reaches a point of 80% or 100% RH where the DBT is very low.

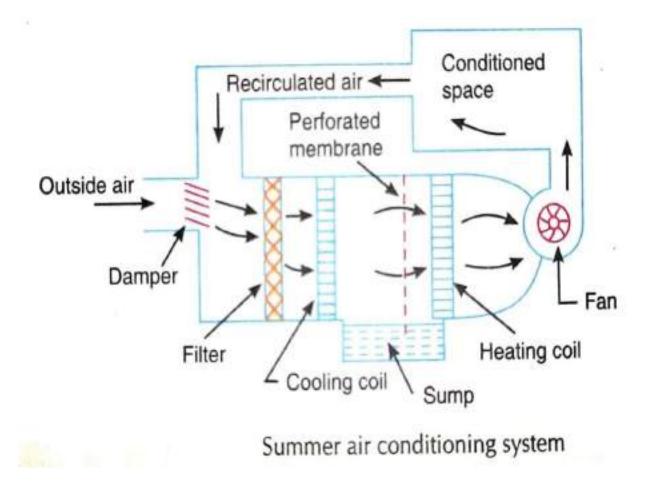
So in order to get the desired dry bulb temperature, again the process of reheating is done where the desired percentage 40% RH is also obtained.

7.A damper is used in order to control the area and have an intake of the required amount of air.

Summer Air Conditioning System:

Initially, during summer, the dry bulb temperature is high and the relative humidity of air is low.

Relative humidity should not be less than 60% according to the comfort conditions for summer air conditioning.



Working of Summer air conditioning system:

1. The outside air(atmospheric air) flows through the air filter to remove impurities or dust particles present in the air. The air now passes through a cooling coil.

2. The coil has a temperature much below the required dry bulb temperature of the air and very high relative humidity in the conditioned space.

So the cooled air is pumped into a dehumidifier, where it loses its moisture in the conditioned space.

3. After that, the air is made to pass through a heating coil which heats the air slightly.

This is done to bring the air to the designed DBT and relative humidity(RH).

4. Now the conditioned air is supplied to the conditioned space by a fan.

From the conditioned space, a part of the used air is exhausted to the atmosphere by the exhaust fans or ventilators.

The remaining part of the used air is again conditioned.

5. The outside air is sucked and it is made to mix with the recirculated air to make up for the loss of conditioned air through exhaust fans or ventilation from the conditioned space.